

Synthesis and application of ion imprinted polymers for selective extraction of metal ions from different matrices

By

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Declaration

I, **Masindi Muphulusi Lizzy** (student number 1130093), hereby declare that this dissertation titled “Synthesis and use of ion imprinted polymers for selective extraction of metal ions from different matrices” for the degree of Master of Science in Chemistry at the University of Venda, this work, which I have submitted, has never been submitted before for credit toward any degree at this or any other university. Both the design and the implementation are wholly unique, and all referenced sources have been correctly cited.



18/02/2024

Candidate signature..... Date

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First and foremost, I am utterly grateful to God Almighty for providing me with the wisdom, courage, grace, and persistence necessary to undertake this study and finish it as best I could. Without his favors, I could not have accomplished this.

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Dedication

This work is devoted to my family, especially my mother (Mavis), Uanea, and Riphuluse, who supported me throughout my Master's program and showed me love and encouragement beyond words.

Abstract

Exposure to toxic metal ions such as Zn^{2+} and Pb^{2+} can lead to several diseases including cancer on human being. This study aims to synthesize Zn^{2+} and Pb^{2+} ion imprinted polymers (IIPs) for removal of Zn^{2+} and Pb^{2+} from various sample matrixes. Polymerization was achieved by mixing the methacrylic acid (MAA) as a functional monomer, ethylene glycol di-methacrylate (EGDMA) as a cross-linker, azobis (isobutyronitrile) (AIBN) as initiator and methanol as a progen. The temperature was increased to 80 °C while stirring for 7 h. The identical procedure was used to make non- imprinted polymer (NIP), but no template was used. Imprinted polymers were extracted with 2 M HCl for the removal of templates.

The point of zero, or $pHPZC$, was determined and infrared spectroscopy was used to characterize the final products. The results of the Fourier-transform infrared (FTIR) analysis demonstrated the removal of ion templates by broad O-H peak at a wavelength of 3500 cm^{-1} and $pHPZC$ results revealed that, at acidic solution, the imprinted polymers carried positive charges, and at basic solution pH, the imprinted polymers carried negative charges the $pHPZC$ was found 6.98 and pH level was 7.0.

The maximum percentage of Zn^{2+} removal using the Zn-IIP was found to be 80% when the solution pH of 7.0, adsorbent dose was 5 mg, contact time at 15 min at shaking speed of 100 rpm and initial metal ion concentration of 25 mg/L were used. The adsorption kinetic data corresponded to pseudo-second order reaction kinetics with $R_2 = 0.99$, indicating that the process occurred by chemisorption. The Langmuir isotherm showed an excellent fit with an adsorption capacity of up to 9.03 mg g^{-1} and $R_2 = 0.99$, implying that adsorption was on a monolayer surface. This study shows that zinc ion imprinted polymer has higher efficiency towards Zn^{2+} in the solution. The finding indicates that zinc ion imprinted polymer has high adsorption efficiency of 94.00 (mg/g) in removing zinc ion from the honey sample.

The removal of Pb (II) from wastewater using Pb (II) IIP was found to be 90%. Further the re-usability study was evaluated 7 times and the adsorption efficiency was high at 90%, for this study the waste material can be beneficial for reused. The functional groups of both the imprinted polymer and the non-imprinted polymer were characterized by FTIR, and the point of zero charge was determined using the optimum conditions of 50 mg adsorbent dose, initial solution pH 9, and 15 min contact time. The adsorptive nature of the IIP and NIP was evaluated by means of Langmuir and Freundlich isotherms. The Langmuir adsorption isotherm modelled

the data better, as shown by the Langmuir and Freundlich correlation coefficients of 0.999 and 0.975, respectively.

An inventive answer has evolved in the form of ion-imprinted polymer, which was produced using the molecular imprinting approach as a basis. Higher selectivity coefficients have been demonstrated by IIPs compared to non-imprinted polymers.

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List of Abbreviations

| | |
|---------|---|
| AAS | Atomic absorption spectrometry |
| ABCN | Azobis cyclohexanecarbonitrile) |
| ATRP | Atom transfer radial polymerization |
| BET | Brunauer-Emmett-Teller |
| BPO | Benzoylperoxide |
| DSPE | Dispersive phase extraction |
| DVB | Divinylbenzene |
| EGDMA | Ethylene glycol dimethacrylate |
| FTIR | Fourier-transform infrared spectroscopy |
| HPLC | High-performance liquid chromatography |
| ICP-OES | Inductively coupled plasma atomic emission spectroscopy |
| ICP-MS | Inductively coupled plasma atomic mass spectrometry |
| IIP | Ion imprinted polymer |
| IOCs | Inorganic contaminants |
| LOD | Limit of detection |
| LOQ | Limit of quantification |
| MAA | Methacrylic acid |
| MIP | Molecularly imprinted polymer |
| MISPE | Molecularly imprinted solid-phase extraction |
| MSPD | Matrix solid phase extraction |
| NMP | Nitroxide-mediated polymerization |
| POPs | Persistent organic pollutants |

| | |
|------|--|
| RAFT | Reversible addition-fragmentation chain transfer |
| SEM | Scanning Electron Microscopy |
| SPE | Solid phase extraction |
| SPME | Solid phase micro-extraction |
| TGA | Thermogravimetric analysis |
| 4-VP | 4-vinylpyridin |

Chapter 1: Introduction

1.1 Background

Global environmental and public health concerns about contamination of all ecosystems by toxic metals have increased in recent years (Okerefor et al., 2020). This is mainly because these toxic metals such as Zn^{2+} , Pb^{2+} and Cd^{2+} are enduring in the surroundings and they might amass and bio-magnify in the environment and contaminate the food web (Ali et al., 2019; Guo et al., 2020; Tamjidi et al., 2020). Moreover, human exposure to toxic metals poses various health risk. For example, cadmium reduces kidney function, lead give rise to memory failures while consuming large amounts of zinc over a long period causes anaemia, nervous system disorders, damage the pancreas and low level of good cholesterol (Alengebawy et al., 2021; Awuchi et al., 2020; Hussain et al., 2012).

The man-made activities have contributed immensely into the availability of these toxic metals into the surroundings (Chen et al., 2021; Dai et al 2019; Duru et al., 2019). For example, Tariq (2021) reported the concentrations of 0.613, 0.316, 0.162, 0.065, 0.041 and 0.028 $mg L^{-1}$ for Ni, Cd, Pb, Cr, Cu, and Zn, correspondingly in the wastewater from industry Zvinowanda et al. (2009) detected Pb, Se, Sr, U and V in groundwater samples which was contaminated by mine wastewater, a study was conducted in South Africa with concentrations ranging from 0.05 – 1.11 mg/L , 0.07 – 0.16 mg/L , 0.15 - 3.40 mg/L , 0.23 – 0.38 and 0.08 – 2.14 mg/L , respectively.

As a natural product, honey's composition varies depending on the location, pollen, honey drew, and nectar source. Natural honey may contain distinct minerals, trace elements and toxic metals at various concentrations (Gałczyńska et al. 2021; Carreck et al., 2020). The research was done in Ethiopia by Adugna et al. (2020) found the toxic metals Cd, Cr, Cu, Mn, Pb and Zn in honey samples with concentrations of 0.017 $\mu g g^{-1}$, 0.15 $\mu g g^{-1}$, 1.15 $\mu g g^{-1}$, 7.29 $\mu g g^{-1}$, 2.53 $\mu g g^{-1}$ and 16.03 $\mu g g^{-1}$, respectively. This amounts are below the permissible limits.

Toxic metals are often found to be above maximum allowable limits in environmental and food samples. It is therefore important to extract these toxic metals as they are harmful to the environment. Toxic metals can now be removed employing a range of methods, encompassing both biological and chemical ones. These methods have several limitations. For example: membrane technique is expensive (Low et al., 2017), chemical precipitation: produce large volumes of sludge, moreover slow metal precipitation and poor settling requires-treatment (Kumar et al., 2019). Aeration techniques is required high capital cost for aeration equipment

(Marsidi et al., 2018). Table 1.1 demonstrates a few techniques that have been employed to eliminate hazardous metals from various environmental media.

Table 1. 1 Removal methods for heavy metals.

| Removal methods | Advantages | Disadvantages | Ref |
|------------------------|--|--|---------------------------|
| Chemical coagulation | Sludge settling | Excessive cost | Bahroodin et al. (2021) |
| | Dewatering | Large consumption of chemicals | |
| Ion exchange | Metal selective | Elevated | Jang et al. (2022) |
| | High treatment capacity | Maintenance cost | |
| Chemical precipitation | Low cost | Disposal problem | Crini & Lichtfouse (2019) |
| | Easy to perform | Sludge is produced in prohibitive cost | |
| Membrane filtration | Membrane is found in distinct size ultrafiltration, nanofiltration and osmosis | Low flow rate Prohibitive cost | Rezakazemi et al. (2018) |

Adsorption is a highly effective method used to remove certain target compounds, such as drugs and other organic compounds, and toxic elements and other ions from various matrices (Khan et al., 2020; Rasheed et al., 2020). The process by which a substance (adsorbate, or sorbate) builds up on a solid surface (adsorbent, or sorbent) is called sorption, more precisely adsorption. The adsorbate binds to the adsorbent whether it is liquid or gaseous. The unsaturated forces of the solid surface to establish bonds with the adsorbate are what propel adsorption. The adsorption process has intrigued many researchers due to its minimal cost and excellent efficiency, and design flexibility (Dey et al., 2021; Pérez-Botella et al., 2022; Velusamy et al., 2021). Adsorption can take two forms: chemical adsorption and physical adsorption. Numerous bonding processes, including hydrogen bonds, van der Waals forces, electrostatic forces, and hydrophobic interactions, are what lead to the physical adsorption process. Adsorbent and adsorbate undergo a chemical reaction that interacts to generate an

electrical connection. (Scheufele et al., 2016). Figure 1.1 shows the general physical and chemical adsorption

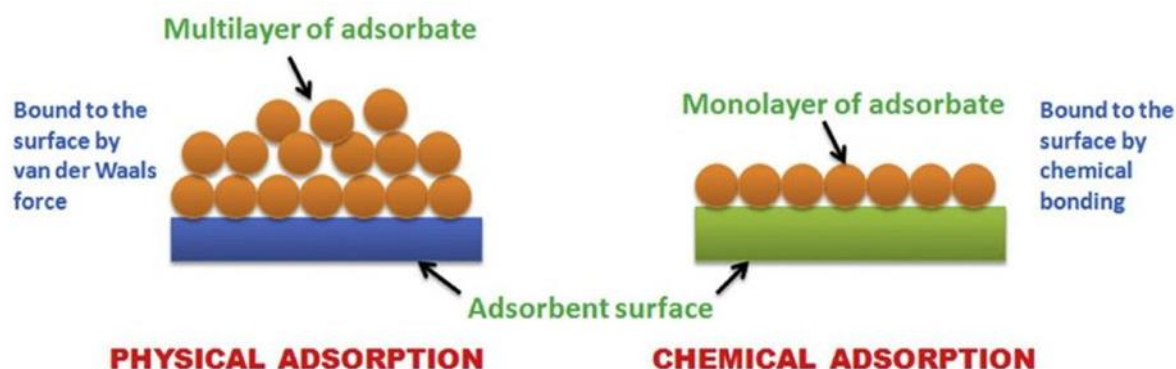


Figure 1.1: General adsorption process

Adsorbents can be natural or manufactured and employed in the adsorption process. Zeolites and clays are examples of natural adsorbents; MIPs and IIPs are examples of synthetic adsorbents. (Alipoori et al., 2021; Zhang et al., 2021).

Ion-imprinted polymers (IIPs) are nano-porous polymeric materials that, in the presence of closely related inorganic ions, can selectively rebind, detect, or transport the target analyte upon leaching the imprint ion. Ion imprinting polymer (IIP) sorbents often improve the selectivity and quality of analytical methods. The first IIPs developed showed their value to separate and identify target ions (Płotka-Wasyłka et al., 2016; Zhou et al., 2018). IIPs are sorbent substances with unique benefits such as stability and selectivity, and are straightforward to prepare and use; consequently, many applications have been developed in analytical methodology. During selection of extraction, pre-concentration and analytical methods, an optimal sorbent should also be chosen to get the highest selectivity for the target ion (Jakavula et al., 2020; Janczura et al., 2018; Shakerian et al., 2016).

Heavy metals nowadays are priority pollutants. To safeguard humans and the environment, these hazardous metals should be eliminated from various matrixes, including wastewater. Ion imprinted polymers were selected as adsorbents for this study because high selectivity, reusability and absorptivity can be achieved by choosing a suitable functional monomer and cross-linker (Lai et al., 2019). The functional monomer and cross-linker used have a significant impact on the steadiness of the polymer intricate generated during the polymerization process as well as the effectiveness of IIPs' interaction with target ions (Zhou et al., 2018). While

methacrylic acid can interact with a template ion by hydrogen bonding, ethylene glycol dimethacrylate is highly reactive and produces polymers with high hardness and stability (Fauziah et al., 2018).

1.2 Problem statement

Inorganic pollutants like zinc, lead, and cadmium have negative health effects causing various health conditions such as cancer, brain damage, kidney disease and lung cancer. The exposure routes which include ingestion, dermal contact and deposition (Alengebawy et al., 2021). These heavy metals matrix include sewage, sludge, weathering, industries and forest fires (Ali et al., 2019). Due to various health conditions, there are methods developed to remove toxic metals in the honey/water which include osmosis, filtration and ion exchange (Chai et al., 2021). Adsorbents that have been used are mineral, organic and inorganic materials which include activated clay mineral, zeolite, farming waste and activated carbon, the challenges regarding this adsorbent include no regeneration, expensive, time consuming and even the sorbent used are not selectivity (Crini et al., 2019). In this research, IIPs (Targeting zinc, cadmium and lead) were synthesized to remove toxic metals in presence of competing ions because of their selectivity, low-cost preparation, easy storage, reusability and long life since other polymers had drawbacks which include sensitivity and binding site can be destroyed during grinding.

1.3. Aim and objectives

1.3.1. Aim

The main aim of this study is to synthesize ion imprinted polymers for application in the extraction of Pb^{2+} and Zn^{2+} from different matrices.

1.3.2. Objectives

- To synthesize ion imprinted Pb^{2+} and Zn^{2+} polymers and further determine their physicochemical characteristics.
- To evaluate the efficiency of the synthesized polymers towards the extraction of Pb^{2+} and Zn^{2+} .
- To model adsorption data using kinetics and adsorption isotherms models.
- To assess reusability of the prepared ion imprinted polymers.

1.4 Research questions

- Can ion imprinted polymers for Zn and Pb be effective in removal of Zn^{2+} and Pb^{2+} ions?
- What is the efficiency of the synthesized ion imprinted polymers in removal of Zn^{2+} and Pb^{2+} ions in different matrices?
- Can the ion imprinted polymers be re-used?

1.5 Significance of the study

Metals are suited to sustainable development goals. They are not biodegradable and have unlimited lifespan including potential recyclability. Heavy metals are eliminated from water and consumer products like honey can prevent damage to the ecosystem and even life-threatening complications such as cardiovascular and neurological conditions.

1.6 Thesis structure

Chapter 1: Introduction and background information.

Chapter 2: Literature review.

Chapter 3: Synthesis, characterization and use of a Zn (II)-IIP to extract and determine Zn (II) in honey.

Chapter 4: Synthesis of a Pb (II) -IIP to selectively extract Pb (II) from wastewater.

Chapter 5: Conclusions and Recommendation

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Chapter 2: Literature review

2.1. Preamble /introduction

Human exposure to toxic metal has long lasting health effects including cancer amongst other diseases due to their persistence in human body and are composed of long life that last for decades (Ayangbenro and Babalola, 2017; Rahman et al., 2019). The prime topic of this chapter is reviewing the occurrence of heavy metals in honey and wastewater, health effects, detection and removal methods and molecular imprinting in details.

2.1.1. Occurrence of trace elements in wastewater and honey

These heavy metals may be found in wastewater because of human or natural activity (Dhaliwal et al., 2020; Sun et al., 2019). Geographical processes like volcanic eruptions, rock weathering, and leaching into rivers, lakes, and oceans are the sources of trace metals in the surrounding (Gautam et al., 2016; Liu et al., 2019; Weldeclassie et al., 2018). Agoro et al. (2020) assessed Cu, Cd, Fe and Pb levels in wastewater and sewage sludge in the Eastern Cape and reported concentrations of 1.17 mg/L, 14 mg/L, 69.789 mg/L and 0.999 mg/L, respectively.

The composition of honey depends on nectar and honeydews, it composed of carbohydrate such as glucose, sucrose, fructose and maltose as well as flavonoid, minerals, vitamins and pollen grains (Pavlova et al., 2018; Bobis et al., 2020). Primary nectar and honeydew are the sources of the mineral components of honey. Honey's mineral content is determined by the minerals that plants naturally absorb from the soil and surrounding environment. It is known that honey pollutes the environment. Because honey bees can travel over an area of about 50 km² and come into interaction with the ground, water, and air, the concentration of trace elements in honey corresponds to the amount of that region (Ogidi et al., 2020; Jovetić et al., 2017). Trace elements are the ash essence of honey, it contains elements such as Zn, Pb and Cd. Zinc is essential for metabolism but at above maximum allowable limit, it is toxic like lead and cadmium (Vetrimurugan et al., 2017). Because bees inhabit broad areas, they are more exposed to chemicals in the environment. contaminants on or in fodder plants, soil, water, and air are reflected in honey. The biological and geographic origin of honey influences the amount of hazardous metals present in it (Mračević et al., 2020). Measurable concentrations of trace elements like Zn (0.76 to 3.41 mg/L), Pb (0.05 to 3.81 mg/L), and Cd (15.00 to 36.40 mg/L) have been detected in honey by Barth et al. (2020).

2.1.2. Health effects

Trace elements have negative impact on human health, for example imbalanced Zn and Cd can interfere with glucose level, potentially leading to cardiovascular diseases (Jomova et al., 2022:

Leal et al., 2023). Trace elements accumulate in brain, heart, liver and kidneys, which are important organs in the human body. The health risk associated with toxic elements depend on the concentration of this elements and the length of exposure (Yousefi et al., 2021). Table 2.1 shows toxicity of metals in honey and wastewater.

Table 2. 1: Metal toxicity of human in wastewater and honey.

| Metal | Toxicity effect | Permissible limit in wastewater (mg L ⁻¹) | Ref | Permissible limit in honey (mg L ⁻¹) | Ref |
|---------|-------------------------------|---|-----------------------|--|-------------------------|
| Cadmium | Lung, liver and kidney damage | 0.10 | Kinuthia et al., 2020 | 0.2 | Aghamirlou et al., 2015 |
| Lead | Lung and liver damage | 5.0 | | 0.3 | |
| Zinc | Anaemia and nausea | 2 | Agoro et al., 2020 | 1 | |

2.2. Detection method

A convenient detection method is needed to monitor heavy metal concentrations. Different methods are used to detect metal in honey/wastewater sample (Bommuraj et al., 2019; Donner et al., 2019; Henriques et al., 2019; Kosek et al., 2019; Sixton et al., 2019). These analyses are most important to guarantee the honey and wastewater purity and safety. Several detection approaches, such as spectrophotometry, electrochemistry, inductively coupled plasma-optical emission spectrometry (ICP-OES) and atomic absorption spectroscopy (AAS), have been developed for heavy metal detection. Some of the techniques are extremely sensitive and precise; Table 2.2 shows various heavy metal detection levels.

Table 2. 2: Methods for detection of heavy metals.

| Methods | Metal detected | Detection level (mg kg ⁻¹) | Sample | Reference |
|--|----------------|--|------------|----------------------------|
| | Cd | 0.005 | | |
| Microwave plasma-atomic emission (MIP-AES) | Pb | 0.123 | honey | Malhat et al., 2019 |
| | Zn | 0.244 | | |
| | Cd | 0.030 | | |
| Atomic absorption spectroscopy (FAAS, GFAAS) | Zn | 14.62 | honey | Adugna et al., 2020 |
| | Pb | 2.53 | | |
| | Zn | 5.39 | | |
| Plasma optical emission spectroscopy (ICP-OES) | Pb | 1.50 | honey | Leblebici and Aksoy (2008) |
| | Cd | 0.24 | | |
| | Zn | 0.1 | | |
| Sensor | Cd | 0.1 | wastewater | Hwang et al., 2018 |
| | Pb | 0.2 | | |

2.3 Removal of toxic metals

Water and honey contamination is a major problem.; therefore, the effective development of suitable methods for extraction of toxic metals in honey and water is necessary.

2.3.1. Chemical precipitation

The transformation of substances dissolved in water into solid particles is known as chemical precipitation. Ionic components are extracted from water by chemical precipitation by adding counter-ions to lessen their solubility (Dayarathne et al., 2021: Priya 2021 et al., Wang et al., 2021).

Numerous variables affect the effectiveness of the chemical precipitation process, such as the kind and amount of ionic metals in the solution, the precipitating agent used, the pH of the solution, and the existence of additional precipitation-related components that could interfere with the reaction (Chen et al., 2018: Sis & Uysal 2014: Wanga et al., 2019: Sun at el. 2020). Table 2.3 shows chemical precipitation methods that were used to remove trace elements.

Table 2. 3: Chemical precipitation removal of heavy metals.

| Heavy metal | Precipitant | Removal efficiency (%) | Reference |
|-------------------|---|------------------------|----------------------|
| Cu and Zn | Lime | 99.65 and 99.00 | Chen et al., (2018) |
| Zn | Vermiculite | 97.00 | Sis & Uysal, (2014) |
| Fe, Cr and Vo | Magnesium hydroxy carbonate | 99.90 | Zhanga & Duan (2020) |
| | Dipotassium salt of 1,3 benzenediamidoethanethiol | 90.00 | Pohl (2020) |
| Hg, Cd, Cu and Pb | Sulfide yeasts | - | Sun et al., (2020) |
| Hg, Pb and Cu | Bicarbonate activated hydrogen peroxide | 78 | Wang et al., (2019) |

2.3.2. Membrane filtration

Membrane filtrations allows water to pass through a membrane materials through a membrane materials due to a pressure difference and remove impurities (Lee et al., 2022; Ling et al 2017; Yang et al., 2019). Water components with a circumference greater than the membrane pore size are deposited on the surface, according to the size of the particles that need to be separated (Gao et al., 2018; Gouda et al., 2023; Lie et al., 2020). The benefits of membrane filtration are that there are no phase changes involved, the feed and product streams stay liquid, the processes can operate efficiently at low temperatures, and there is little energy required. The drawbacks of membrane filtration are that the processes are susceptible to membrane fouling effects, which cause the permeate flux to decrease, and costly cleaning and regeneration schemes may be required (Aktij et al., 2020; Hube et al., 2020). The high flow rates of cross-flow feed may shear sensitive materials It might be expensive to purchase equipment. Inadequate performance during separation may arise if the membrane production process is not properly managed, from membranes with a significant pore size dispersion (Afome at al., 2019; Germikli et al., 2020). Table 2.4 shows membrane filtration removal methods of heavy metal including removal efficiency.

Table 2. 4: Membrane filtration removal method of heavy metals.

| Membrane | Heavy metal | Medium | Removal efficiency | Reference |
|--------------------------------------|-----------------------|----------------|--------------------|-------------------------|
| Nano fibrous metal organic framework | Pb | Wastewater | 18-37 % | Efome et al., (2019) |
| PAN/PANI-nylon core-shell nanofibers | Pb | Aqueous | 87.57 % | Almasion et al., (2018) |
| | Cd | solution | 86.00 % | |
| Polymer | Pb, Cd and Cu | wastewater | 90.00 % | Cao et al., (2018) |
| Cu-ETDA | Cu | wastewater | 71.40 % | Li et al., (2020) |
| <i>N</i> -methyl-D-glucamine | As and B | Water | 86.00 % | Çermikli et al., (2020) |
| Cellulose nitrate | Cd, Co, Cu, Ni and Pb | Water and food | 95.00% | Gouda et al., (2023) |

2.3.3 Adsorption

A material (adsorbate, or sorbate) is gathered surface-level of a strong material (adsorbent, or sorbent) through the process of adsorption. Adsorbate may exist in a gaseous or liquid phase. Unsaturated strengths at the strong surface that can frame bonds with the adsorbate are the driving constraint for adsorption (Basu et al., 2021; Han et al., 2022; Abu Taleb et al., 2022). Usually, these advantages are reversible or electrostatic (van der Waals intelligent). Coordination of the irreversible electron exchange between the sorbent and the sorbate is a more pragmatic intuitive concept. The nature of this interaction determines how easy or difficult it is to expels (desorb) the adsorbate in order to recover the adsorbent and retrieve the adsorbate. The degree of surface contact and relative accessibility of a single component in a bolster blend determine the unique character of the adsorbent (Lonappan et al., 2018). The allocation between the liquid and strong stages serves as the isolating instrument, and the strong is the mass-separating operator. To invert the process and recover the sorbent, an energy-separating operator is used, usually a weight or temperature change. Adsorbents are categorized into three categories: natural, agricultural, and synthetic (Chakroborty et al., 2022; Ghorbani et al., 2020; Osagie et al., 2021; Syafiuddin et al., 2020; Xue et al., 2022). Because of their high effectiveness, metal recovery, generative nature, and economy, these adsorbents are found to be encouraging in the removal of toxic metals (Jatoi et al., 2021). Molecular imprinted polymers and ion imprinted polymers, which fall within the molecular imprinting category, are examples of synthetic adsorbents (Balouch et al., 2019; Liang et al., 2020). The capacities a selection of the adsorptive materials used to extract heavy metals are shown in Table 2.5.

Table 2.5: Adsorbents used to remove heavy metals.

| Metal ion | Adsorbent | Adsorption capacity (mg/g) | Reference |
|-----------|-----------------------|----------------------------|-------------------------|
| Cu and Pb | Porous lignin | 276.00 and 332.00 | Wang et al., (2020) |
| As | Iron CS microspheres | 120.70 | Lebo et al., (2020) |
| As | Magnetic CS coated GO | 45.00 | Sherlala et al., (2019) |
| Cd | CS- pectin gel beads | 117.60 | Shao et al., (2021) |
| Cd | CS- based hydrogels | 234.80 | Viela et al., (2019) |
| Pb and Cd | Coconut waste | 263.00 and 285.00 | |
| Hg | Black oak bark | 400.00 | Alalwan et al., (2020) |
| Cr | Wheat brans | 310 | |
| Fe and Zn | Rambutan peels | 17.40 and 14.00 | Low et al., (2023) |
| Pb | Ion imprinted polymer | 40.02 | Huang et al., (2019) |

2.4. Molecular imprinting

Molecular imprinting was first discovered by Polyakov (1931). He polymerized silica carbonate in the presence of a specific porogen (e.g., xylene or toluene) and the resulting silica demonstrated preferential binding capacity for the solvent in the solution. Frank Dickey (1955) polymerized silica gels when dyes are present and observed that silica prepared in the presence of one of several dyes showed higher selectivity than with other dyes (Lofgreen & Ozin, 2014).

After two decades of the MIPs discovery, there was a decrease in the study of molecular imprinting of silica because of the introduction of the organic molecular imprinting. Cross-linker was introduced in 1972 to improve the adsorption capacity by Takagish and Kotz. In the 1970s and 1980s, Wulff's group published many papers of organic MIPs capable of selective adsorption of enantiomers of glyceric acid. Mosh and Arshady (1981) reported organic ion imprinted polymer that was prepared using non-covalent approach.

By using a process called molecular imprinting, polymers with unique recognition sites that are made to resemble a target ion or molecule in terms of size, shape, or functional group can be produced (Amatatongchai et al., 2019; Dar et al., 2020; Zouaoui et al., 2020). The functional monomer and the template must form a complex in order for this process to proceed, which is then followed by polymerization and cross-linking. Various methods can be used to remove the template after synthesis, such as extraction by high-pressure hot water, organic solvents, or microwave irradiation (Sun et al., 2017, Wang et al., 2018; Zhang et al., 2021; Liang et al., 2020; Zhu et al., 2021). As a result, the resulting MIPs bind to the template and similar molecules in a mixture only because their binding sites are compatible with the template (Herrera-Chacón et al., 2021).

Ion imprinting techniques are derived from the MIP technique, using an ion instead of a molecule. Nishide et al. (1976) reported the metal ion imprinting by complexing with Hg^{2+} , Ni^{2+} , Zn^{2+} , Co^{2+} , Cu^{2+} and Cd^{2+} with poly(4-vinylpyridine) and 1,4-dibromobutene as monomer and cross-linker respectively. Figure 2.1 schematically shows the principles of the polymerization process.

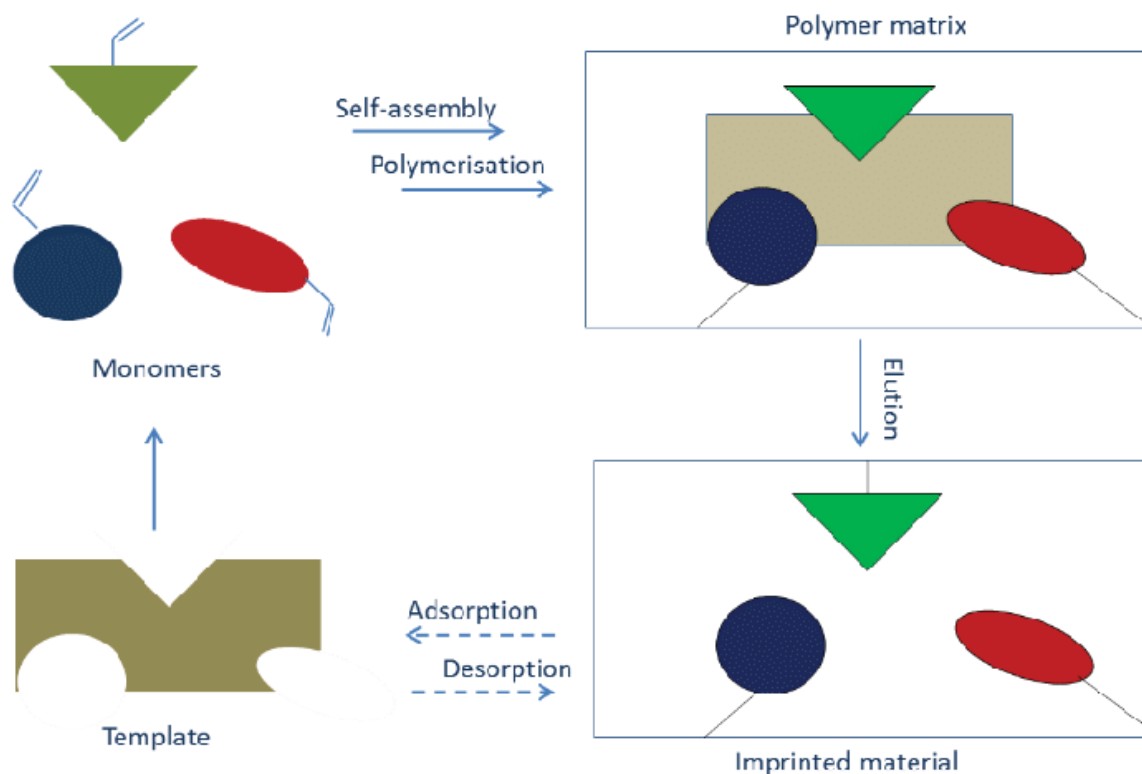


Figure 2.1: General principle of imprinting polymers.

2.5. Components of IIPs

2.5.1. Template

The template molecule is crucial in ion imprinting processes, as its ion structure dictates the selection of a useful monomer for synthesis. The chemical bonds between the template and functional monomer are essential for successful ion recognition (Suriyanarayanan et al., 2017). Under the circumstances of polymerization and synthesis, it is critical that the template be stable and chemically inert (Sun et al., 2017).

2.5.2. Functional monomer

Functional monomers are responsible for creating recognition sites on the imprinted polymer by their interaction with the template molecule (Mier et al., 2021). Selection of an appropriate functional monomer determines the structure of the binding site, and the quantity of monomer used affects the number of recognition sites. However, an excessive amount of functional monomer can cause non-specific adsorption site formation on the ion imprinted polymer (Chen et al., 2020; Polyakova et al., 2016). The bond between the monomer and ion can be either covalent or non-covalent, and it plays a crucial role in achieving a highly selective recognition site (Zhang et al., 2021). Figure 2.2. Shows examples of functional monomers.

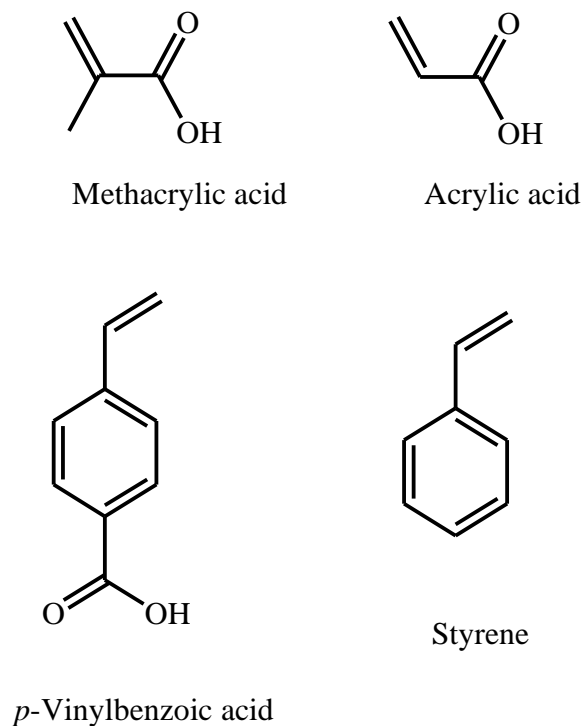
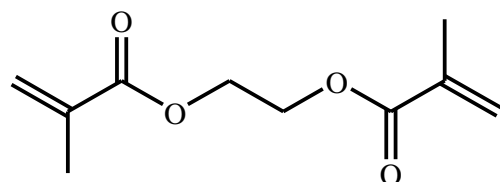


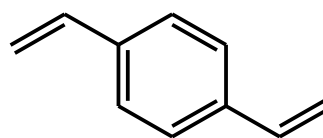
Figure 2.2: Structure of common function monomers.

2.5.3. Cross-linker

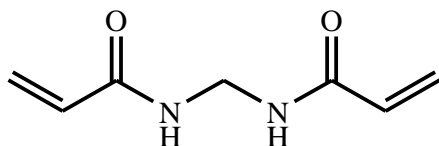
The primary functions of a cross-linker are to (i) regulate the polymer matrix morphology, (ii) enhance the stability of the binding sites formed by imprinting, and (iii) provide mechanical strength to the polymer matrix (Ersoy et al., 2016; Mahani et al., 2021). During polymerization, a higher ratio of cross-linkers is generally favoured to achieve good porosity (Masoumi et al., 2021). Figure 2.3 illustrates commonly utilized cross-linkers.



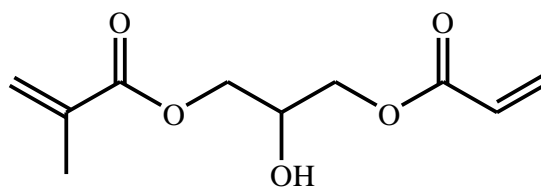
Ethylene glycol dimethacrylate



Divinylbenzene



N,N'-Methylenebisacrylamide



3-(Acryloyloxy)-2-hydroxypropyl methacrylate

Figure 2.3: Examples of IIP cross-linkers.

2.5.4. Solvent (porogen)

Porogens are solvents employed in the polymerization process, wherein they must be able to dissolve the template, cross-linker, functional monomer, and initiator. The polarity of the porogen contributes to the replacement of the template with the functional monomer (Liu et al., 2019; Madikizela et al., 2016).

2.5.5. Initiator

The initiator promotes reaction during polymerization. The initiator generates radicals during its decomposition to initiate reaction (McKenzie et al., 2019). Figure 2.4 shows examples of initiators.

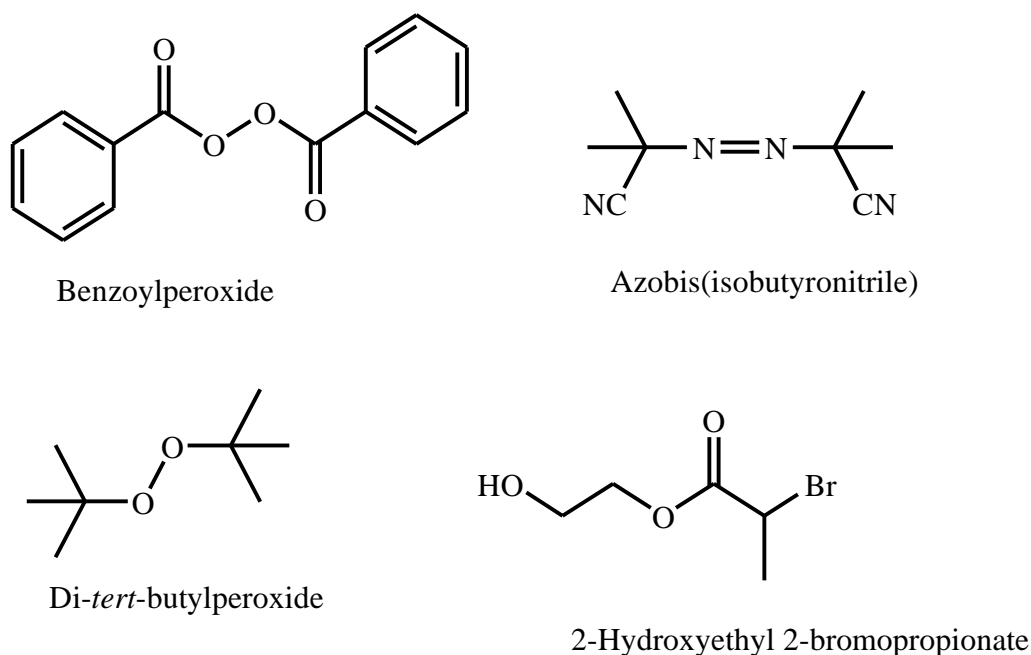


Figure 2.4: Commonly used initiators.

2.6. Imprinting approaches

Imprinted polymers can be synthesized using three distinct approaches: covalent, non-covalent, and semi-covalent.

2.6.1. Covalent approach

In the covalent approach, a chemical connection develops between a functional monomer and the template molecule by sharing electrons before the polymerization process. This is depicted in Figure 2.5 (Xie et al., 2021). Elution, or the separation process, is achieved through a chemical reaction where the obtained imprinted polymers (IIPs) selectively rebind to the template molecule via covalent interactions. The monomer/template complex remains stable, and various conditions can be employed in this approach (Hasanah et al., 2021).

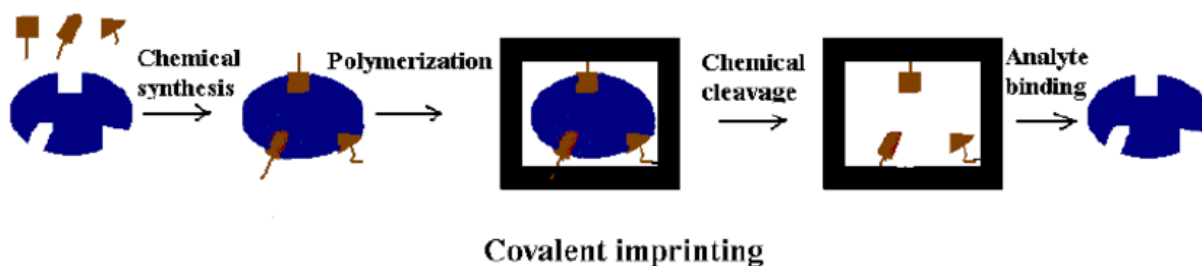


Figure 2.5: Covalent ion imprinting (Yan et al., 2006).

2.6.2. Non-covalent approach.

The non-covalent approach entails the establishment of weak interactions like van der Waals forces or hydrogen bonds, and between the template and an appropriate monomer before polymerization. This is achieved by mixing the template and monomer together (Kumar et al., 2021; Shen et al., 2021). Elution of the template is accomplished by solvent washing. This approach is widely employed due to its advantages, including easy preparation and efficient removal of the template from the polymer (Zhang et al., 2021). Figure 2.6 illustrates a general depiction of non-covalent imprinting.

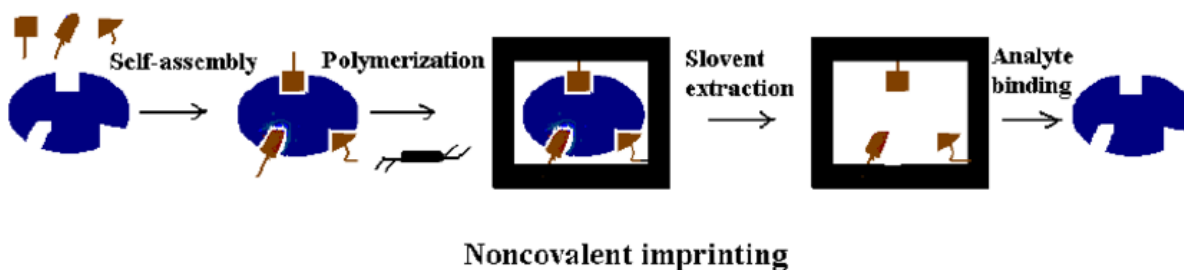


Figure 2.6: Non-covalent ion imprinting (Yan et al., 2006).

2.6.3. The semi-covalent approach

This method incorporates components from the non-covalent and covalent techniques. It involves the capacity of the template to rebind with the polymer, akin to non-covalent imprinting, and the production of a stable and stoichiometric complex, akin to covalent imprinting (Jacob et al., 2018).

2.7. Polymerization mechanisms

2.7.1. Free radical polymerization

Under particular reaction conditions, one method for performing free radical polymerization is when a solution or in bulk. Three steps are involved in the mechanism of free radical polymerization: initiation, propagation, and termination.

2.7.1.1. Initiation

Chain initiation in free radical polymerization occurs in two stages. First, an initiator is dissociated, resulting in formation of free radicals, as depicted in Figure 2.7. The second stage involves the addition of a monomer to these free radicals. Benzoyl peroxide and 2,2'-azo-bis-(isobutyronitrile) (AIBN) are commonly used as radical initiators (Liang et al., 2019; Pirman et al., 2021). Both compounds usually dissociate into two one-electron radicals. These radicals react with an alkene monomer by forming a new bond with one of the electrons of the alkene monomer, while the remaining electron becomes a new free radical (Hussein et al., 2020; Mavrouidakis et al., 2021).

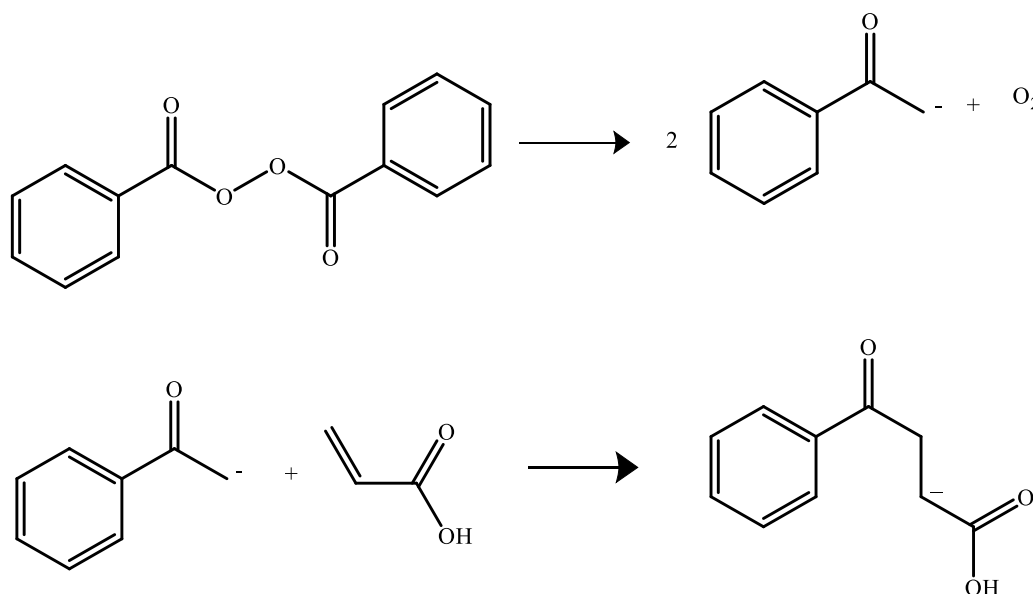


Figure 2.7: Schematic representation of initiator decomposition.

2.7.1.2. Propagation

Propagation in free radical polymerization refers to the continuous polymer chain lengthening by the continuous reaction of monomers with the active (radical) centres. This addition of each monomer occurs rapidly, typically within a millisecond. Within a minute, thousands of monomer additions can occur (Mueller et al., 2014).

2.7.1.3. Termination

Termination in free radical polymerization refers to the deactivation of the radical active centres. At this point, two mechanisms could happen: combination and disproportionation. Combination is the process of joining two expanding strands to create a single polymer chain. Conversely, disproportionation is the process of moving a hydrogen atom from one polymer chain to another, which creates distinct end groups. Zhang et al. (2014) and Konkolewicz et al. (2013).

2.7.2. Controlled radical polymerization) using reversible addition-fragmentation chain transfer agent

One of the most popular and adaptable synthesis techniques is called RAFT (Reversible Addition-Fragmentation Chain Transfer) polymerization (Hu et al., 2020). According to Gyorgy et al. (2021) and Yildiko et al. (2021), it has a number of benefits, such as (i) compatibility with a broad range of monomers, (ii) operation at mild conditions, (iii) feasibility of polymerization by various methods, and (iv) fine control over the material structure. The qualities of IIPs are improved by this technique.

2.8. Formats of IIPs

Imprinted polymers (IIPs) can be fabricated in various formats using different techniques, depending on their intended applications. The choice of format and fabrication technique directly impact the adsorption capacity and the accessibility of binding cavities within the IIPs.

2.8.1. Bulk polymerizations

Bulk polymerization, sometimes referred to as mass polymerization, uses a reaction mixture without a porogen (solvent) that consists of a monomer and a soluble initiator. In this combination, polymerization occurs. After that, grinding and sieving procedures are usually used to the resultant polymer (Suzuki et al., 2012; Wang et al., 2019).

2.8.2. Emulsion polymerization

A polymer in the form of monodispersed particles, usually with a size range of tens to hundreds of nanometers, is produced via emulsion polymerization. An oil-in-water emulsion is typically used in this procedure, where the monomer droplets, which function as the oil phase, are distributed throughout a continuous water phase. During polymerization, stable emulsion droplets are formed.

2.8.3. Suspension polymerization

Suspension polymerization is a process that creates polymers by vigorously stirring a polymeric reagent into a solvent. This procedure causes monomer droplets to separate, which then creates a homogeneous suspension and ultimately produces polymer beads (Trojanowska et al., 2017).

2.8.4. Precipitation polymerization

When monomers and cross-linkers in a homogeneous system experience radical initiation, polymerization takes place. Chain propagation then takes place, creating a polymer network that precipitates in an unsuitable solvent. A narrow size distribution of polymer particles is formed as a result of the precipitation process, without the use of any stabilizer or surfactant (Sajini and Mathew, 2021; Nishizawa et al., 2020). Figure 2.8 provides an overview of the general polymerization process involved.

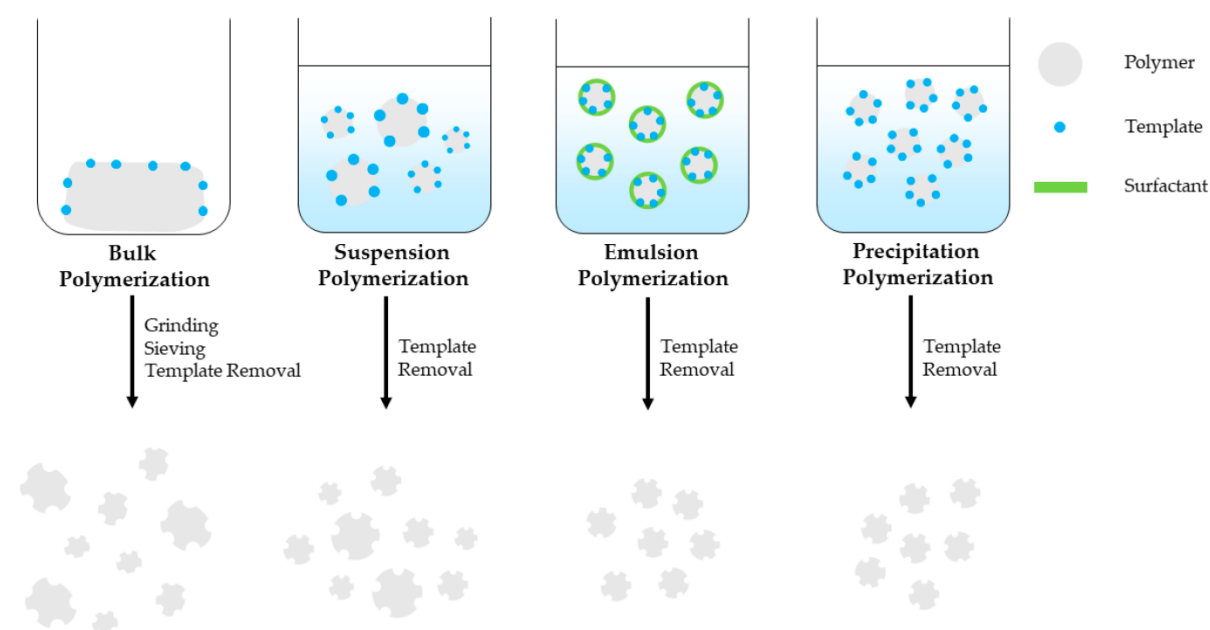


Figure 2. 8: Polymerization process

2.9. Application of IPPs

Among the applications of IIP are catalysis and synthesis reactions, selective extraction, the removal and separation of contaminants from biological and environmental samples, chemical analysis, and the detection of metal ions in a variety of materials.

2.9.1 Sensors

Electrochemical and optical sensors are among the newer applications for IIP polymers. IIP polymers are being used as recognition elements in a new generation of electrochemical sensors that produce signals (Sala et al., 2022; Wang et al., 2021). Polymer particles are inserted into a PVC film or a mixture of carbon powder to construct the electrochemical sensor as a modified ion-selective electrode. Optical sensors have also been made using IIP polymers. Cu(II) ions and Al(III) have been detected using optical sensors based on IIP polymers. Modified glass carbon electrode (GCE) Pt(IV) ions in the catalyst and plant samples were detected using an ammeter using the Pt-IIP film made via in situ polymerization.

2.9.2. Membrane

Thanks to developments in polymer science, membrane technology—which includes wastewater treatment, food processing, and environmental applications—is showing great promise. Ion-imprinted membranes, or IIMs, have drawn particular interest as a result (Yu et al., 2022; Zeng et al., 2019; Chen et al., 2022). Their easy operation, low energy and time consumption, and convenient preparation are their defining features. Several initiatives have been made to enhance the mechanical stability, flexibility, and hydrophilic and hydrophilic permeability of membranes. Certain metal ions, for example, are too tiny to be efficiently recovered or separated using IIM porous methods; instead, membrane adsorption and polymer-reinforced ultrafiltration have been developed. There have been several approaches put forth for creating polymeric films imprinted with metal ions (Ma et al., 2017; Xia et al., 2018; Zahid 2018). Modulation Zn(II)-IIM is done by applying the water-in-oil (W/O) emulsion polymerization surface printing process. Crown ether is used as a functional monomer and lithium as a model ion in the surface method imprint polymerization of Ag nanoparticles to create a nanocomposite membrane imprinted with ion (IINcMs). IIM can also be prepared in a single step without the need for extra crosslinking mixing using an effective and straightforward approach (Zhang et al., 2020; Eddaif et al., 2019). By directly combining poly(vinylidene fluoride) (PVDF) with metal-polymer complexes including matrix ions and amphoteric copolymers, selective Pt(IV)IIM films were created. Despite developments in membrane preparation techniques, there is only one. They are known to have a few real-world uses. Layer-by-layer self-assembly technology (LbL) is used to create Cu(II) surface Ion-imprinted composite films (Liu et al., 2019; Zhang et al., 2019).

Pre-concentration, analyte conversion, or the removal of any interferences are typically required steps in analytical methods. These steps ensure that the analyte is in a form that is

appropriate for the detection method. Solid phase extraction (SPE) is one of the many separation techniques used for this purpose, and analysts are particularly interested in it because of its simplicity, adaptability, ease of automation, and small size (Arabi et al., 2020; Faraji et al., 2019). Excellent quality options in the realm of selective absorption are offered by advanced IIP material. When competing ions are present, printing alters the printed material's ion recognition behavior, which is reflected in the polymer's selectivity. In addition, IIP polymers are helpful in speculative analysis due to their strong affinity for metallic forms. Robust adsorption IIP's capacity to remove harmful metals from biological fluids and purify various hazardous substances contaminated surface water and wastewater is advantageous (Guo et al., 2017; Zheng et al 2020).

IIP is applicable to both dynamic and static processes. Analytes can be effectively separated from a variety of materials using the static approach, which involves leaving the absorbent in making contact with the sample for a set period of time (Larki et al., 2021; Xie et al 2020). A magnetic magnet can be used to solve the absorbent and solution separation issue. IIP layers and an external magnet are used to cover the nanoparticles (Hemmati et al., 2018; Mendeles et al., 2020). The dynamic method's benefits include its simplicity of use, low reagent requirements, quick separation times, and wide range of adsorbent applications (He et al., 2017; Tang et al., 2020). Moreover, the sample integration and miniaturized pre-treatment made possible by the IIP online flow system enable the detection of analytes utilizing sensitive spectroscopic techniques (Yu et al., 2020; Faraji et al., 2019).

Primarily uses of IIP deal with the separation of metal ions that are extremely harmful to living things, such as Tl(III), CH₃Hg(I), Pb(II), Cd(II), and Hg(II), before identifying them using various methods. Traces of Cd(II) have been extracted from food, water, and serum samples using polymers imprinted with the metal (Hu et al., 2021; Wang et al., 2019). Because heavy metal ions have a low affinity for ion exchange resin, heavy metal removal from wastewater treatment is challenging (Fu et al., 2022; Li et al., 2017). The most efficient method for removing Cd(II) and Hg(II) ions from wastewater has been determined to be a random copolymer of methacrylate and metha-crylamide (Wang et al., 2020; Zhao et al., 2018).

2.10. Summary

It is important to synthesize material for treating honey and wastewater, since natural adsorbent are not selective like coconut but to synthesize a new material which is specified for certain trace elements it would be better and the removal efficiency will increase. Commercial honey

also contains trace elements but most of them are below maximum allowable limits. Most of the adsorbent that are present have low removal percentage of trace element due to low specificity and selectivity, most of this adsorbent can be used once and are not economic efficiency since some of the reagents are expensive.

Due to their high specificity and selectivity, stability under extreme conditions, extended shelf life, and economic efficiency they can be reused over seven times with removal efficiencies above 80% ion imprinted polymers provide several appealing features.

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Chapter 3: Synthesis, characterization and use of zinc (II) IIP to remove trace elements from honey

Abstract

This chapter aims at synthesizing zinc ion imprinted polymer to remove zinc selectively from honey in the presence of competing ions. A Zn(II)-IIP and an Zn(II)-NIP were obtained by a precipitation reaction. The Zn(II)-NIP and Zn(II)-IIP were characterized by infrared spectroscopy to assess the functional groups present and absent, while surface charges were evaluated based on the pH point of zero charge. The efficiency of the synthesized polymers towards selective adsorption of Zn (II) was evaluated through batch adsorption experiments. The maximum percentage of Zn²⁺ removal using the Zn-IIP was found to be 80% when the solution pH of 7.0, adsorbent dose was 5 mg, contact time at 15 min at shaking speed of 100 rpm and initial metal ion concentration of 25 mg/L were used. The adsorption kinetic data corresponded to pseudo-second order reaction kinetics with $R^2 = 0.99$, indicating that the process occurred by chemisorption. The Langmuir isotherm showed an excellent fit with an adsorption capacity of up to 9.03 mg g⁻¹ and $R^2 = 0.99$, implying that adsorption was on a monolayer surface. This study shows that zinc ion imprinted polymer has higher efficiency towards Zn²⁺ in the solution. The finding indicates that zinc ion imprinted polymer has high adsorption efficiency of 94.00 (mg/g) in removing zinc ion from the honey sample.

Keywords: Ion imprinted polymer, zinc, precipitation polymerization and atomic absorption spectroscopy

3.1. Introduction

Honey is a natural saturated sugar solution which contains nutrients and carbohydrate. Honey is used as a food preservative (Haber et al., 2019). It contains enzyme, proteins, vitamins, lipids, flavonoids and minerals (Abdelnour et al., 2019). The honey's quality depends on the climate conditions, production methods, nectar source and processing and storage conditions (Pavlova et al., 2018). Trace metals such as cadmium, nickel, and lead, metals like zinc, copper, and chromium have been reported previously in honey samples (Squadrone et al., 2020). It is important to ensure that the levels of these metals in honey remain below the maximum allowable limit, as they play integral roles in human health and development (Adugna et al., 2020; Altundag et al., 2016). Intake of essential metals (Zn and Cu) when are above the maximum allowable limits can cause chronic disease (Varol et al., 2017). Trace metals comes

from anthropogenic sources like industrial pollution and improper procedure during maintenance stage and process of honey (Aljohar et al., 2018; Hermanns et al., 2020).

Zinc nutrient it is enforced for processes like cellular metabolism, DNA synthesis, gene expression, catalytic activity, immune function protein synthesis, cell division and wound healing (Lin et al., 2018; Maret et al., 2013; Fontana et al., 2017). Zinc is found naturally in plants and in certain foods, such as shellfish, pork, and beef. It can also be added to other foods and is available as a dietary supplement. Cold lozenges and some over-the-counter cold remedies also contain zinc. Zinc plays a role in supporting normal growth and development during pregnancy, childhood, and adolescence, as well as maintaining a proper sense of taste and smell. The body does not have a specialized storage system for zinc, so a daily intake of 40 mg is necessary to maintain a steady state. Excessive intake of zinc, above this requirement, can lead to symptoms like nausea, vomiting, and anaemia. Analytical methods, such as AAS, ICP-OES, and ICP-MS, have been developed to detect trace levels of zinc (II) in biological, pharmacological, food, and environmental samples. Stecka et al. (2014) and Aduga et al. (2020) used these methods and reported concentrations ranging from 0.13 to 15.38 $\mu\text{g g}^{-1}$ and 9.96 to 16.03 $\mu\text{g g}^{-1}$, respectively.

It is important to remove zinc from honey because it can cause indigestion, vomiting and diarrhoea, and over the long term it causes low immunity and low copper levels. Different methods have been applied in extraction such as osmosis, ion exchange, filtration, electrolysis and adsorption (Charles et al., 2016; Thaçi and Gashi, 2019). Compared to other methods, the adsorption method is highly efficient and flexible (Azha et al., 2021). Carbon nanotubes, clay, and zeolite are known adsorbents for removing metals (Burakov et al., 2018; Zhou et al., 2019). However, there is still a need for low cost-effective adsorbents. This is where molecular imprinting comes in, offering a promising method with remarkable capabilities. Molecularly imprinted polymers (MIPs) have a permanent memory for the template, so that they can re-bind the target molecule selectively in a mixture of similar compounds. MIPs and ion-imprinted polymers (IIPs) differ in their recognition substance, which can be an ion or molecule. IIPs are a group of highly selective materials that can recognize specific ions even when competing ions from intricate matrices are present. (Sun et al., 2017).

In the process, the initiator undergoes splitting, resulting in the formation of initiator fragments that contain unpaired electrons known as free radicals (Nishizawa et al., 2020; Qin et al., 2018). These unpaired electrons then pair with ethylene glycol dimethacrylate (EGDMA), which is

referred to as the initiation step. During the propagation step, additional monomers are added to the growing chain. Finally, in the termination step, the two unpaired electrons join to give a polymer (Hu et al., 2020; Tian et al., 2018).

We describe the synthesis, characterisation, and use of Zn-IIP for solid phase extraction-based zinc pre-concentration in this study. Atomic absorption in flame was used to analyze the quantity of zinc. Using zinc sulphate as a template, methacrylic acid as a functional monomer, and ethylene glycol di-methacrylate as a cross-linker, the IIPs were created. FTIR was used to study the IIP's characterization. Investigations were done on the experiment's parameters, including sample pH, concentration, and flow rate. The trace amount of zinc (II) ion was enriched using this approach from an aqueous solution.

3.2. Material and methods

3.2.1. Chemicals and reagents

Methanol (99%), methacrylic acid (MAA) (99%), azobisisobutyronitrile (AIBN) (98%), ethylene glycol dimethacrylate (EGDMA) (99%), hydrochloric acid (99%) and zinc sulphate (99%) were sourced from Merck (Wadeville, South Africa). Cobalt (II) chloride (97%), copper (II) sulphate (98%), manganese (II) chloride tetrahydrate (99%), nickel (II) chloride (99%) and iron chloride (98%) were bought from Sigma-Aldrich. All the chemicals were analytical grade.

3.2.2. Synthesis of ion imprinted polymers (IIPs)

The synthesis of IIPs was carried out according to the modified procedure of Xia et al. (2017). To 70 mL ethanol (in a 250 mL one-neck round-bottomed flask), 0.116 g (0.5 mmol) $ZnSO_4$ was added as template and 422 μ L (5 mmol) MAA monomer were added. To eliminate oxygen and create an inert environment, the mixture was stirred for 15 minutes. Following that, 2 mL (10 mmol) EGDMA was introduced. Before adding 50 mg (0.3 mmol) AIBN as the initiator, the solution was purged with nitrogen for 2 minutes to eliminate oxygen. After adding the initiator, the flask was greased with oil and loosely closed loosely with lead and enclosed in parafilm. The flask was heated for 7 h in an oil bath at 80°C, and the product was then cooled, filtered and dried overnight. The NIPs were prepared similarly but without addition of a template.

3.2.3. Elution process

After polymerization, the IIPs and NIPs obtained were each washed 8 times with 2 M HCl to remove the ion template from the polymer. The 3 g IIP and 1 g NIP obtained, were transferred to 50 mL solid phase cartridges with a cotton wool plug in the bottom. The elution process was done in continuous mode. The eluted fractions were collected after every hour. The procedure was repeated eight times for both IIPs and NIPs. The wet IIPs and NIPs were then dried for overnight. Figure 3.1 shows synthesis of Zn (II) imprinted polymer

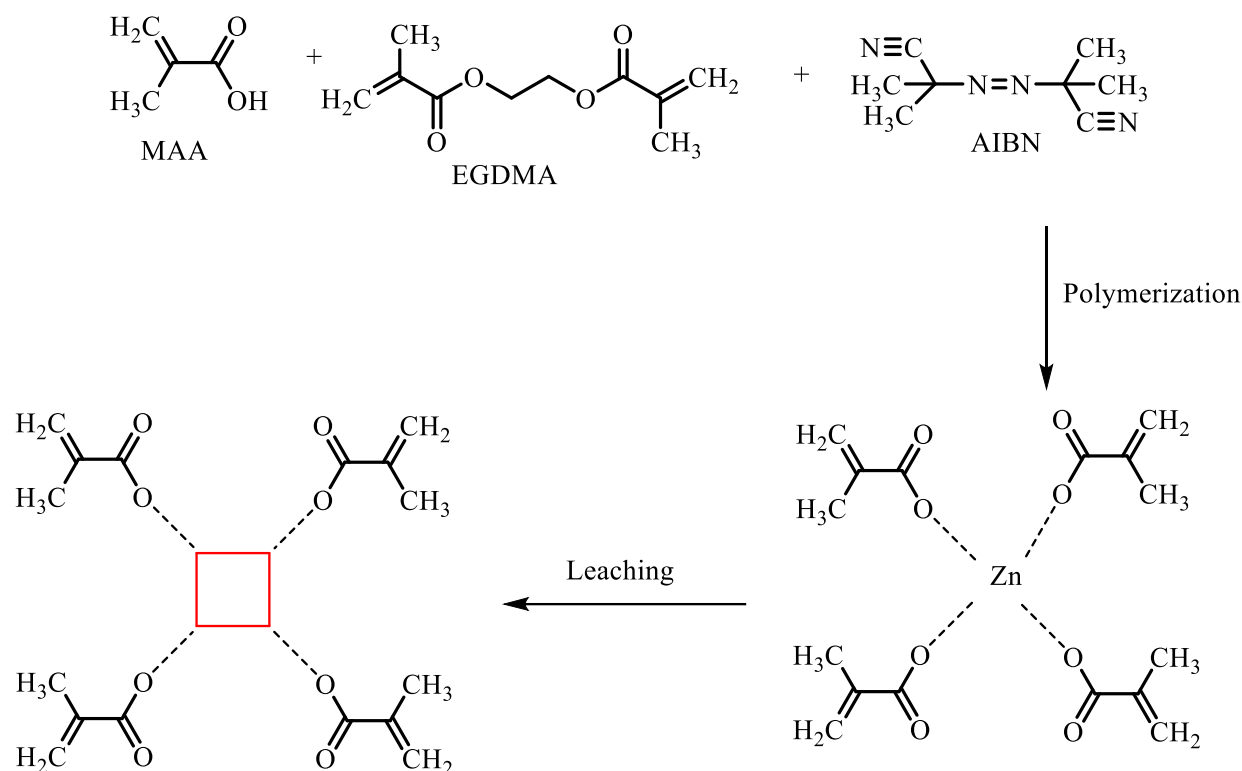


Figure 3.1: Illustration of the imprinting process to produce a Zn (II) imprinted polymer.

3.2.4. Adsorption studies

The batch adsorption experiments involved varying the parameters sample pH, temperature, contact time, mass, metal ion concentration, and shaking speed. A univariate analysis approach was employed, wherein one variable was altered while keeping the other parameters constant. To adjust the solution pH, 0.1 mol L⁻¹ NaOH/HNO₃ was used, and for each adsorption experiment, the solutions were subsequently filtered. The resulting mixture was filtered, and the concentration of the filtrate was determined using atomic absorption spectroscopy (PinAAcle 900T from PerkinElmer). The percentage adsorption, E, and equilibrium adsorption capacity Q_e (measured in mg/g) were calculated using the following formulas:

$$E = \frac{C_i - C_f}{C_i} \quad (3.1)$$

$$Q_e = \frac{(C_i - C_f) V}{W} \quad (3.2)$$

where C_i and C_f = the respective initial and final concentrations of Zn (II) (mg L^{-1}),

W = sorbent weight (g), and

V = solution volume (mL).

3.2.4. Surface area measurement

A 0.01 g L^{-1} Methylene Blue standard solution was prepared and a calibration curve drawn at $\lambda = 600 \text{ nm}$ using UV-VIS spectroscopy. To calculate surface area, 0.1 g IIP was treated with 25 mL Methylene Blue solution until the absorbance was constant.

The surface areas of the Zn-IIP and NIP were determined using the formula

$$A_s = \frac{G \cdot N_{av} \cdot \theta \cdot 10^{-20}}{M \cdot M_W} \quad (3.3)$$

where A_s = the surface area of the imprinted polymer ($\text{m}^2 \text{ g}^{-1}$),

G = the amount methylene blue adsorbed (g),

N_{av} = Avogadro's number ($6.02 \times 10^{23} \text{ mol}^{-1}$),

θ = the cross-section of the methylene blue molecule (197.2 \AA^2),

M_W = the methylene blue molar mass (373.9 g/mol), and

M = the adsorbent mass (g).

3.2.5. Determination of pH_{pzc}

The point of zero charge (pH_{pzc}) was determined by the method proposed by Tavengwa et al. (2016) with a few modifications. Aliquots of 50 mL 0.01 M KCl solution were placed in different 50 mL centrifuge vials and adsorbent was added to each of them before the pH was adjusted with 0.1 M HCl or NaOH solution. After shaking the vials for 15 h at 100 rpm , the mixtures were filtered and the filtrate pH was measured; the pH_{pzc} value is the point where the curve pH_{final} vs $\text{pH}_{\text{initial}}$ cross, i.e. where $\text{pH}_{\text{final}} = \text{pH}_{\text{initial}}$.

3.2.6. Adsorption isotherm

A Zn^{2+} concentration range of 10 to 35 mg/L was used to evaluate the adsorption capacity. To the solution, 5 mg of Zn-IIP or NIP particles were added. The solution pH was adjusted to seven with 0.1 M NaOH or HCl, and it was then shaken at room temperature for 1 hour. After filtration, the Zn(II) concentration in the filtrate was measured using AAS. Adsorption isotherm are important for describing how the adsorbate ion interact with the surface adsorption site and represents the connection between the adsorbate on the surface of the adsorbent at equilibrium and constant temperature and the adsorbate in the surrounding phase (Chenn et al., 2022; Hu et al., 2023). Langmuir, Freundlich and Temkin isotherm models were used to explain the adsorption isotherms.

The Langmuir equation can be expressed as;

$$\frac{C_e}{q_e} = \frac{1}{q_{\max} b} + \frac{C_e}{q_{e \max}} \quad (3.4)$$

where q_e = amount of adsorbate ($mg\ g^{-1}$) at equilibrium,

C_e = ion concentration in the solution

q_{\max} = maximum sorption capacity

b = Langmuir constant

The Freundlich isotherm is suitable for surfaces that are heterogeneous, as it describes surface heterogeneity and the exponential distribution of activation energies:

$$\log q_e = \log K_F + \frac{1}{n} \log C_e \quad (3.5)$$

where K_F = Freundlich constant ($mg/g)/(mg/L)^n$ and n is the exponent of the Freundlich model ($0 < n < 1$).

$1/n$ = adsorption intensity. The value $1/n$ is also a measure of the site heterogeneity.

According to the Temkin isotherm model, the heat of adsorption of each molecule in the layer should fall linearly with coverage rather than logarithmically.

$$q_e = \frac{RT}{b} \ln(A_T C_e) \quad (3.6)$$

$$q_e = \frac{RT}{b_T} \ln A_T + \frac{RT}{b_T} \ln C_e \quad (3.7)$$

$$B = \frac{RT}{b_T} \quad (3.8)$$

$$q_e = B \ln A_T + B \ln C_e \quad (3.9)$$

where A_T = Temkin isotherm equilibrium binding constant ($L g^{-1}$)

b_T = Temkin isotherm constant

R = universal gas constant (8.314 J/mol/K)

T = Temperature (298 K)

B = Constant related to heat of sorption (J/mol)

3.2.7. Adsorption kinetics

The time to completely adsorb Zn^{2+} onto the IIPs was determined. A range of Zn-IIP and NIP samples was prepared by immersing 5 mg of the polymer in 20 mL of a 25 mg/L Zn(II) solution. Over a 5-35 min time interval the samples were filtered through a membrane filter, and the metal concentration was measured using AAS. Possible adsorption mechanisms and reaction pathways that can be characterized by either a pseudo-first order or a pseudo-second order model are provided by the study of kinetics. According to this mechanism, at greater sorbate/sorbent ratios, the kinetics of the adsorption process correspond with two competing reversible second order reactions, and at lower sorbate/sorbent ratios, with reverse second order reactions. Equations (3.9) Pseudo first-order and (3.10) Pseudo second-order define the models.

$$\ln(q_e - q_t) = \ln(q_e - k_1 t) \quad (3.10)$$

$$\frac{t}{q_t} = \frac{1}{k_2 (q_e)^2} + \frac{1}{q_e} t \quad (3.11)$$

where q_t and q_e = adsorption capacity ($mg g^{-1}$) of Zn (II) at time t and at equilibrium, respectively

k_1 = rate constant (min^{-1}) obtained from the pseudo-first order model,

R^2 = linear regression correlation coefficient obtained from a linear plot,

k_2 = rate constant ($g min^{-1} mg^{-1}$) for the pseudo-second order model at equilibrium, and

$k_2 q_e$ and the corresponding linear regression correlation coefficient R^2 are obtained from the linear plot.

3.2.8. Selectivity studies

The selectivity study was conducted under optimized conditions for both the IIP and the NIP. The IIP or NIP (5 mg) was added to an aqueous solution of Zn^{2+} , Cd^{2+} , Pb^{2+} , and Ni^{2+} ions, each at a concentration of 2 $\mu\text{g/mL}$. These competing ions were chosen due to their identical charge, comparable ionic radii, and frequent coexistence with Zn^{2+} ions.

To achieve a sample pH of 7, 0.1 M HCl and NaOH solutions were used for adjustment. The resulting mixture was placed in a 50 mL centrifuge tube and stirred at 100 rpm for 15 minutes. After stirring, the mixture was filtered and the ion concentrations in the filtrate were measured using atomic absorption spectroscopy (AAS). The experiment was repeated three times to ensure reliability and reproducibility. The polymer was filtered using a membrane filter before further analysis. The Zn (II) distribution ratio's (K_d), selectivity factors (K), and relative selectivity factors (K') with regard to Cd (II), Pb (II), and Ni (II), were calculated using Eqs. 3.11–3.13:

$$K_d = \frac{(C_i - C_f)V}{C_f M} \quad (3.12)$$

$$K = \frac{K_{d(\text{Zn(II)})}}{K_{d(\text{competing ions})}} \quad (3.13)$$

$$K' = \frac{K_{\text{imprinted}}}{K_{\text{non-imprinted}}} \quad (3.14)$$

where C_i = initial concentration (mg L^{-1}),
 C_f = final concentration (mg L^{-1}),
 V = ion solution volume (mL), and
 M = sorbent mass (g).

3.3. Preparation of honey sample

Processed honey samples were purchased from a local farm in Levubu, Limpopo, South Africa. The sample was kept at 4°C until analysis. Table 3.1 shows the physico-chemical properties of the honey sample. Processed honey samples were digested following the procedure developed by Adugna et al. (2021). Briefly, in a 250-mL conical flask, 2:1 (v/v) of nitric acid and hydrogen peroxide respectively were added to 10 g of honey sample. The mixture was

subjected to evaporation until it became dry, followed by cooling to reach room temperature. Di-ionised water was added to the cooled sample and filtered. The solution was diluted with additional solvent to reach the 100-mL mark on a volumetric flask. The honey solution was analysed for selected heavy metals Cu, Fe, Ni, Zn, Pb, Mn and Co using atomic absorption spectroscopy. The honey sample pH was adjusted to 7 and the metal concentration in the solution was measured using atomic absorption spectroscopy (AAS) both before and after the addition of a spike.

Table 3.1: Physico-chemical properties of a honey sample.

| Physio chemical properties | Value before digested | Value after digested |
|------------------------------------|-----------------------|----------------------|
| Sample pH | 4.6 | 5.2 |
| EC (ms cm^{-1}) | 2.00 | 2.19 |
| TDS (mg/L^{-1}) | 300.67 | 322.97 |
| Temperature ($^{\circ}\text{C}$) | 28 | 25 |

3.3.1. Application of Zn-IIP in treatment of honey

A 5-mg quantity of zinc ion imprinted polymer (Zn-IIP) was introduced into a centrifuge tube containing 10 mL of honey solution. The mixture was then shaken at a speed of 100 rpm for 1 hour. Afterward, the concentration of the extracted ions was measured.

3.3.2. Sample analysis

The parameters for the instrument were set up as shown above in Table 3.2. The whole procedure was done in triplicate.

Table 3.2: Parameters of AAS determination.

| Parameter | Cu | Fe | Ni | Zn | Pb | Mn | Co |
|-----------------|--------|--------|--------|--------|--------|--------|-------|
| Wavelength (nm) | 324.75 | 248.33 | 232.00 | 307.59 | 283.31 | 279.48 | 240 |
| Current (mA) | 15 | 30 | 25 | 14 | 10 | 20 | 30 |
| Slit (nm) | 0.7 | 0.2 | 0.2 | 0.7 | 0.7 | 0.2 | 0.2 |
| Lamp type | C-HCL | C-HCL | C-HCL | C-HCL | C-HCL | C-HCL | C-HCL |

| | | | | | | | |
|---------------|----|----|----|----|----|----|----|
| <i>Energy</i> | 88 | 62 | 55 | 40 | 82 | 70 | 67 |
|---------------|----|----|----|----|----|----|----|

3.4. Results and discussion

3.4.1. Infrared spectra

The FTIR spectra of both Zn NIP and Zn IIP were measured and are presented in Figure 3.2. Specific absorption bands were observed in the spectra. The band at 2945 cm^{-1} is due to methyl C-H stretching. The band at 1725 cm^{-1} is due to the carbonyl vibration of EGDMA. The presence of C-O-C stretching (ester) is shown by the absorption at 1141 cm^{-1} , while the weak absorption at 1637 cm^{-1} represents C=C bonds. Additionally, a band at 945 cm^{-1} corresponds to C-H bending. The intense broad band observed at 3374 cm^{-1} indicates the presence of O-H groups. In the washed IIP spectrum, this O-H band becomes more pronounced due to the elution of the template, indicating the opening in the polymer structure. Notably, no IR bands were observed in the range of $1500\text{-}1600\text{ cm}^{-1}$, which suggests that the polymerization process is complete. This finding is in line with earlier research that used a new aminothiols monomer to synthesize and characterize a highly selective polymer imprinted with mercury (II) (Firouzzare et al., 2012). and polyethylene glycol's molecular weight has an impact on the production and characteristics of aqueous polyurethane dispersions (Mumtaz et al., 2013).

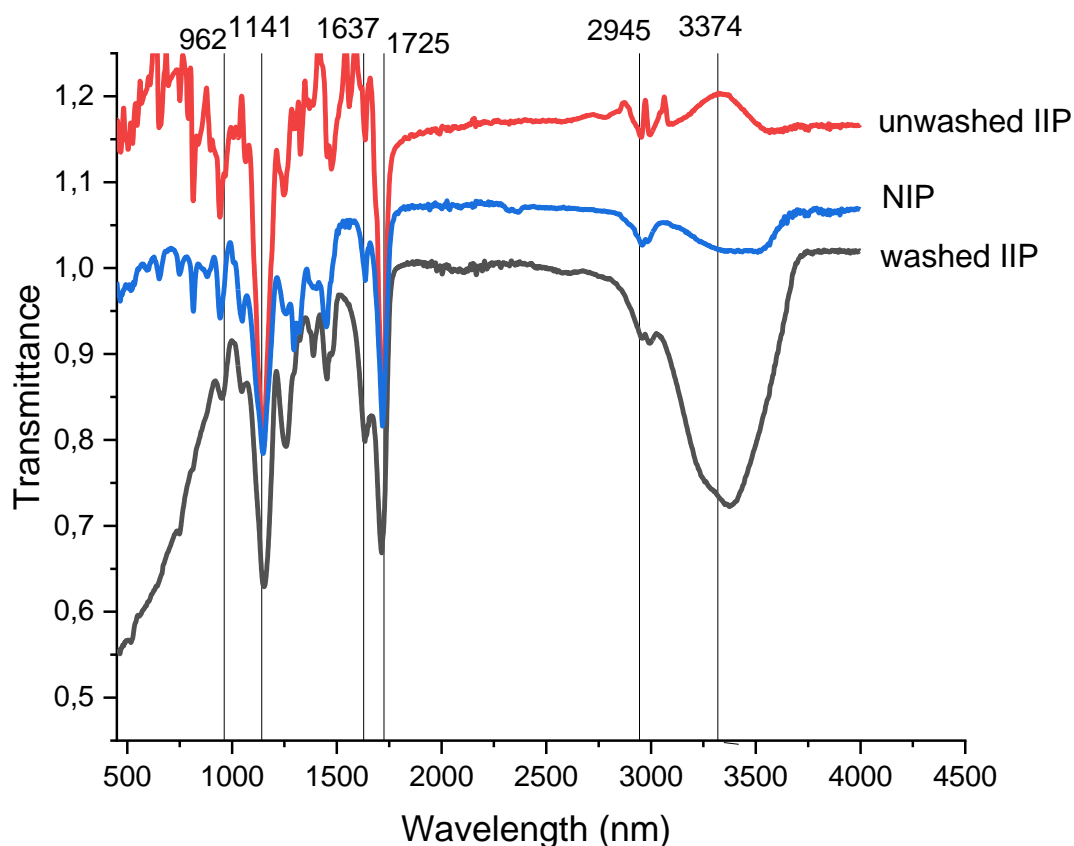


Figure 3.2: Infrared spectra of zinc (II) NIP and Zn (II) IIP washed and unwashed.

3.4.2. Measurement of surface areas

The Methylene Blue adsorption studies showed that leached Zn-IIP had a greater surface area than NIP. This difference in surface area is attributed to the leaching of Zn^{2+} ions out of the polymer, leading to the formation of specific cavities within the polymer network. The adsorption capacity of IIP and NIP is shown in Table 3.2.

Table 3.3: Specific surface areas of synthesized polymers.

| Metal ion | Surface area ($m^2 g^{-1}$) | |
|-----------|-------------------------------|-------|
| | IIP | NIP |
| Zn^{2+} | 15.02 | 12.34 |

3.4.3. Optimization of zinc uptake

3.4.3.1. Effect of solution pH and point of zero charge

Figure 3.3 shows the effect of solution pH on the Zn (II) adsorption efficiency; in acidic medium, it was low, but with increasing solution pH the adsorption of Zn (II) increased, attaining a maximum at pH 7 and then decreasing at higher pH. Figure 3.4 shows the point of zero charge, where H^+ or OH^- are absorbed and the polymer surface has zero net charge, found at pH 6.98. At low sample pH (≤ 6.98) zinc exists as Zn^{2+} coordinating with H_2O , which dissociates to form a proton and hydroxide; at this stage the Zn^{2+} species carry positive charge. At lower sample pH, the repulsive force between particles that are caused by their electric charges which influence adsorption efficiency to be low. At higher sample pH, species have negative charges during adsorption of Zn^{2+} , so that instead of adsorbing it was forming $Zn(OH)_2$ which caused the adsorption efficiency to decrease. Equation 4.15 and 4.16 shows the reaction of zinc and water at lower and high sample pH.

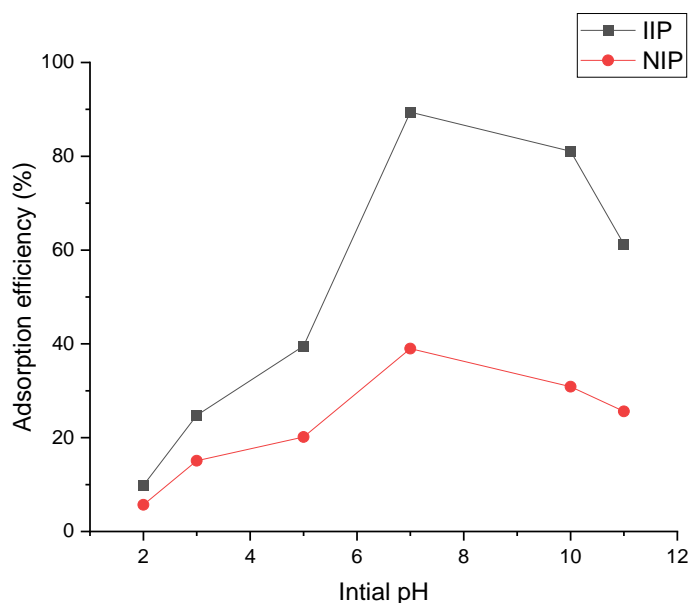


Figure 3.3: pH effect on adsorption of Zn(II) on Zn(II)-IIP and NIP. Conditions: adsorbent mass = 10 mg, initial Zn(II) concentration = 5 mg/L, contact time = 20 min, Shaking speed = 60 rpm at room temperature

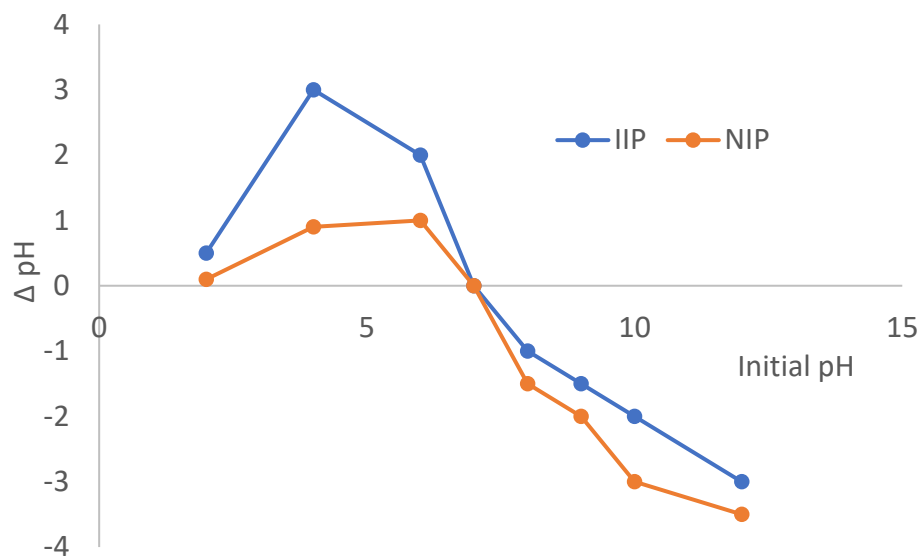


Figure 3.4: Point of zero charge of Zn (II). Conditions: 5 mg adsorbent, Shaking speed 100 rpm for 15 h.

3.4.3.2. Effect of dosage

Figure 3.5 demonstrates the impact of the adsorbent quantity on Zn (II) ion adsorption using the Zn(II) IIP and NIP. The % adsorption efficiency increased up to 5 mg adsorbent mass, after which the adsorption percentage remained constant. The increase in adsorption efficiency up to 5 mg adsorbent can be ascribed to the increase in the number of adsorption sites, increasing the availability of the template to the polymers. The following constant % adsorption efficiency was due to excess vacant sites. Non-imprinted polymer showed the same trend as ion imprinted polymer but the % adsorption efficiency was less because it had no Zn (II) specific binding sites. The optimal dosage was therefore 5 mg, in agreement with Memon et al. (2017), who also noted that increasing the mass of the ion-imprinted polymers provided more binding sites within the polymer, leading to enhanced adsorption efficiency. However, the adsorption efficiency reached its equilibrium point at a mass of 5 mg, which was identified as the optimal mass (Memon et al., 2017).

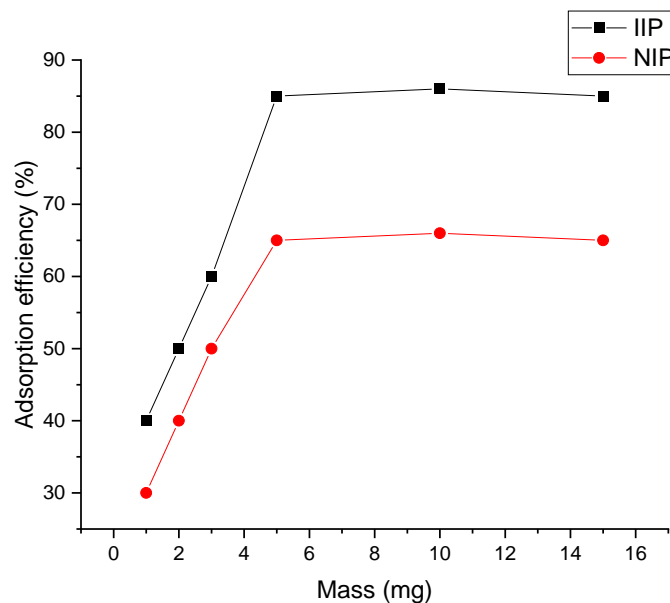


Figure 3.5: Influence of adsorbent mass on adsorption of Zn (II). Conditions: Sample pH = 7, initial concentration = 5 mg/L, contact time = 20 min, and shaking speed = 60 rpm at room temperature.

3.4.3.3. Effect of shaking speed

Figure 3.6 shows the influence of shaking speed on adsorption of zinc (II) onto Zn (II) IIP and NIP. The adsorption efficiency increased with increasing shaking speed. At low shaking speed, the Zn (II) was unable to reach the polymer binding sites. At higher shaking speed, the adsorbate was moving too fast forming the bubbles instead of adsorbing it was desorbing due to this, adsorption efficiency decreased with the increase in shaking speed. NIP adsorption efficiency was low compared to the one for IIP since there was no cavity pore created. Maximum adsorption efficiency was observed at 100 rpm. According to Memon et al. (2017), the adsorption efficiency increased with the increase in shaking speed until it reaches its maximum adsorption at 100 rpm.

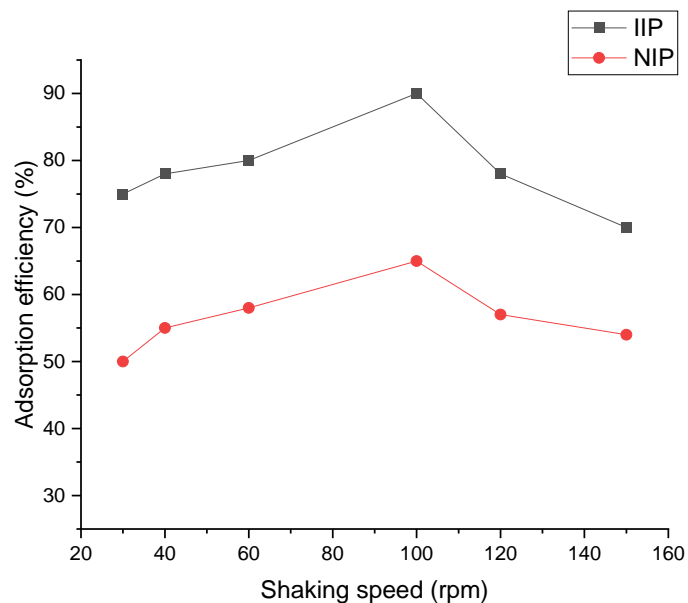


Figure 3.6: Effect of shaking speed on zinc adsorption. Conditions: Sample pH =7, contact time = 20 min, adsorbent mass = 5 mg, and initial ion concentration = 5 mg/L at room temperature.

3.4.3.4. Influence of contact time

The adsorption efficiency increases with an increase in contact time, as presented in Figure 3.7. The adsorption efficiency increased up to a maximum was reached at 15 min; this increase was due to the vacant sites available in the IIP. After 15 min, the adsorption efficiency remained constant because the vacant sites were saturated.

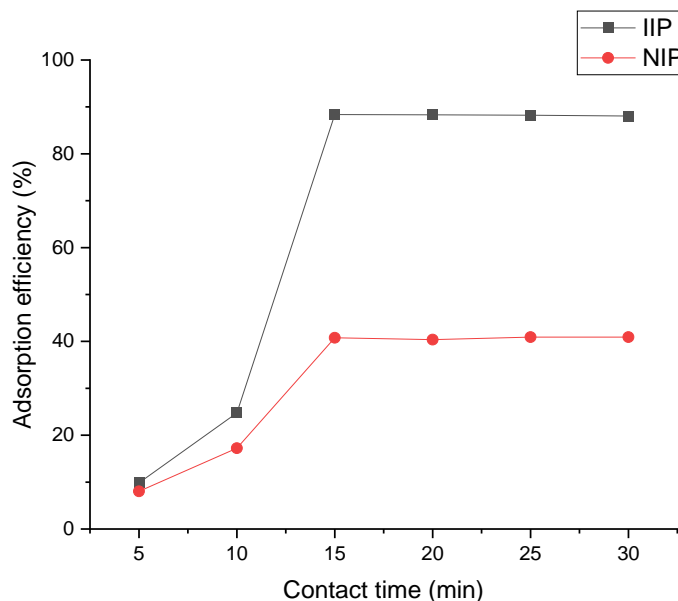


Figure 3.7: Effect of contact time on adsorption. Conditions: Sample pH = 7, initial Zn(II) concentration = 25 mg/L, adsorbent mass = 5 mg, and shaking speed = 100 rpm at room temperature.

In addition to providing data on the adsorption rate, the study of kinetic modeling sheds light on a suitable reaction mechanism. Table 3.4 displays the findings from the kinetic investigations. The pseudo-first-order kinetic model does not well fit the adsorption kinetic data, as evidenced by its lower R^2 value and the notable differences between the estimated and observed adsorption capacities. Conversely, the R^2 values of the pseudo-second-order kinetic model were nearer to one, indicating a superior match to the experimental data. There was a good agreement between the estimated and experimental values of adsorption capacity (q_e) for various initial concentrations of Zn (II) ions. These results suggest the pseudo-second-order kinetic model for Zn (II) ion adsorption onto the ion imprinted polymer. This suggests that the rate-limiting step is most likely chemical sorption, or chemisorption, and that the adsorption rate is more dependent on the adsorption capacity than the concentration of the adsorbate. Other ions cannot be adsorbed at the same location once one ion has been adsorbed there.

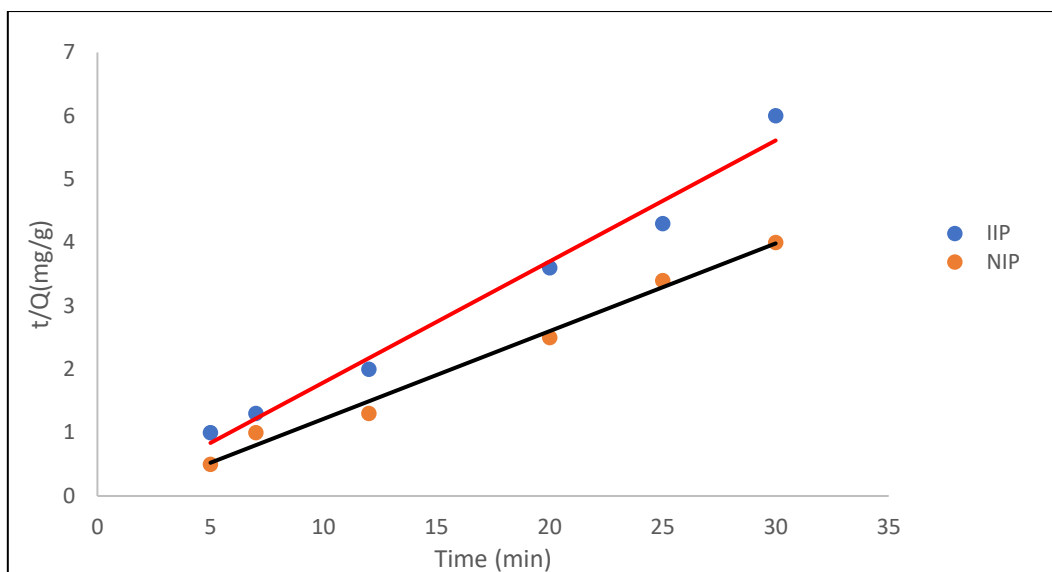


Figure 3.8: Pseudo-second-order kinetics of adsorption of Zn (II) ions by Zn(II) IIP/NIP.

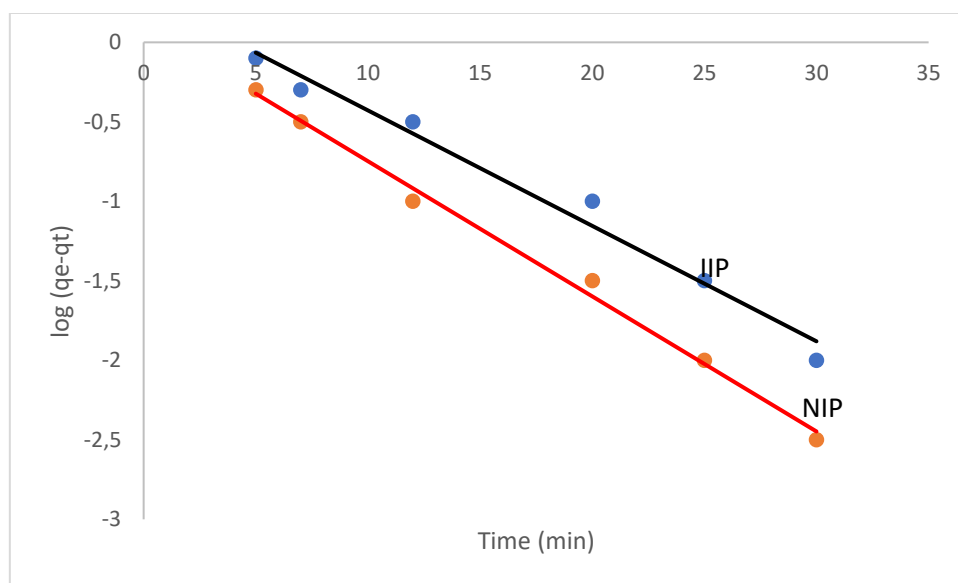


Table 3.4: Constant values for the kinetics models.

| Zn (II) Concentration | q_e exp | K₁ | q_e | R² | K₂ | q_e | H | R² |
|----------------------------------|------------------------------|---------------------------|----------------------|----------------------|----------------------|----------------------|-------------------|----------------------|
| (mg L⁻¹) | (mg/g) | (min⁻¹) | (mg/g) | | (g/mg.min) | (mg/g) | (mg/g.min) | |
| 100 | 4.067 | 0.060 | 1.354 | 0.770 | 0.0424 | 4.245 | 0.696 | 0.999 |
| 100 | 3.023 | 0.031 | 0.985 | 0.584 | 0.0243 | 2.546 | 0.371 | 0.976 |

3.4.3.5. Effect of zinc concentration on the adsorption isotherm

The effect of zinc concentration on adsorption is shown in Figure 3.8. A higher starting concentration resulted in higher adsorption rates, according to the sigmoidal relationship observed in the adsorption rate. Because there were more adsorption sites on the IIP, the first removal % fell as the starting concentration increased. At a Zn(II) ion concentration of 10 mg/L, the maximum adsorption efficiency of 98% was achieved, suggesting that Zn (II) had saturated the surface of the IIP. The fact that the adsorption was unaffected by additional concentration increases suggests that the polymer had achieved its saturation point, which was dependent on the starting concentration.

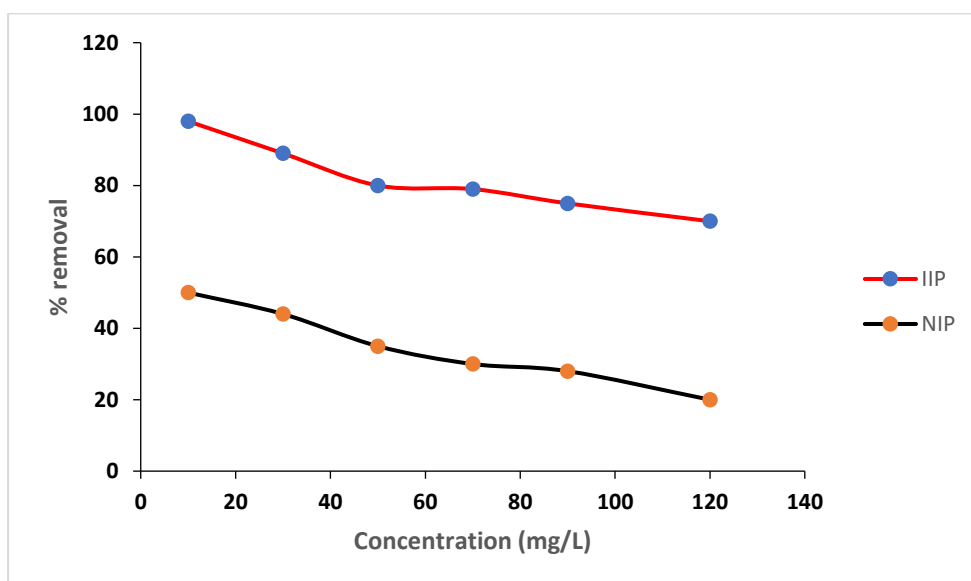


Figure 3.9: Effect of zinc concentration on adsorption. Conditions: Sample pH =7, adsorbent mass = 5 mg, contact time = 20 min, shaking speed = 100 rpm at room temperature.

Langmuir, Freundlich, and Temkin are depicted in Figures 3.10, 3.11, and 3.12, respectively. Using the Langmuir, Freundlich, and Temkin isotherms, the mechanism of zinc adsorption was investigated further (Table 3.5). Zinc adsorption onto both Zn-IIPs and the NIP matched better to the Langmuir adsorption isotherm, suggesting monolayer adsorption, according to an analysis of the Freundlich, Temkin, and Langmuir plots. The Langmuir isotherms model postulates that once the adsorption sites on the homogenous surface were occupied, no more adsorption could take place. The greater correlation coefficient (0.99), as opposed to the values of 0.90 and 0.68 obtained with the Temkin and Freundlich isotherm investigations, respectively, supports the fitting to Langmuir, which was validated by (Table 3.3).

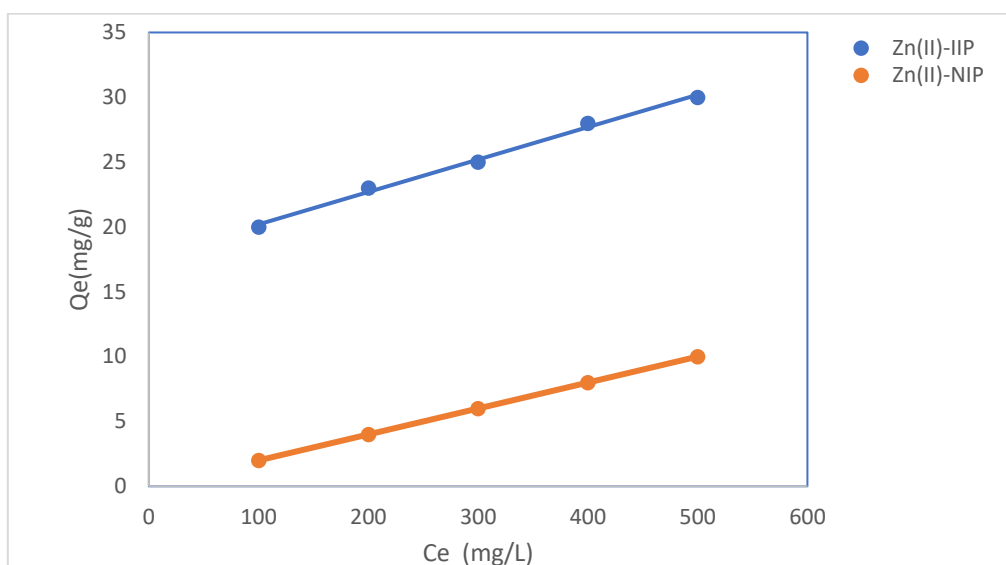


Figure 3.10: Langmuir adsorption isotherm for the adsorption of Zn (II) onto IIPs.

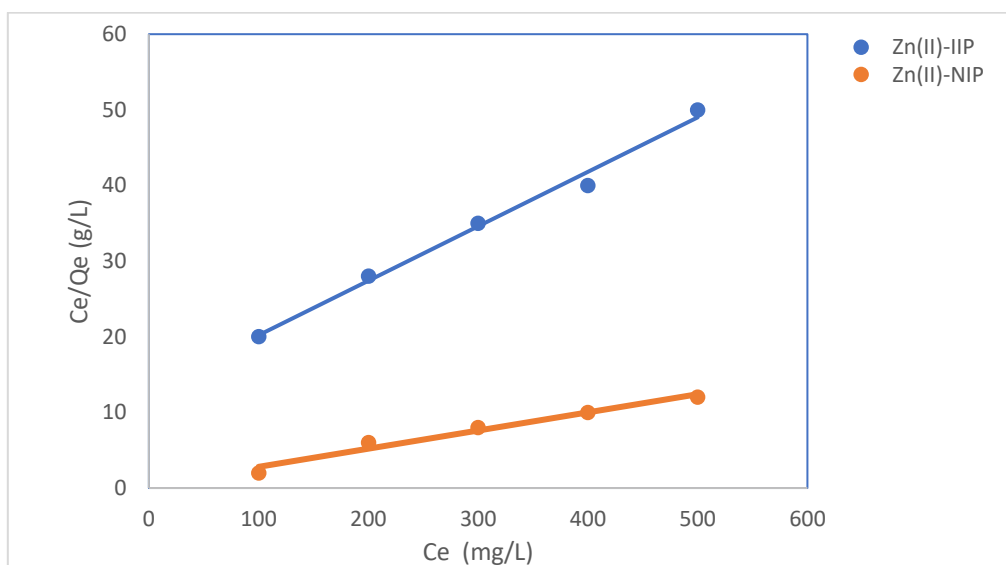


Figure 3.11: Freundlich adsorption isotherm for the adsorption of Zn (II) onto IIPs.

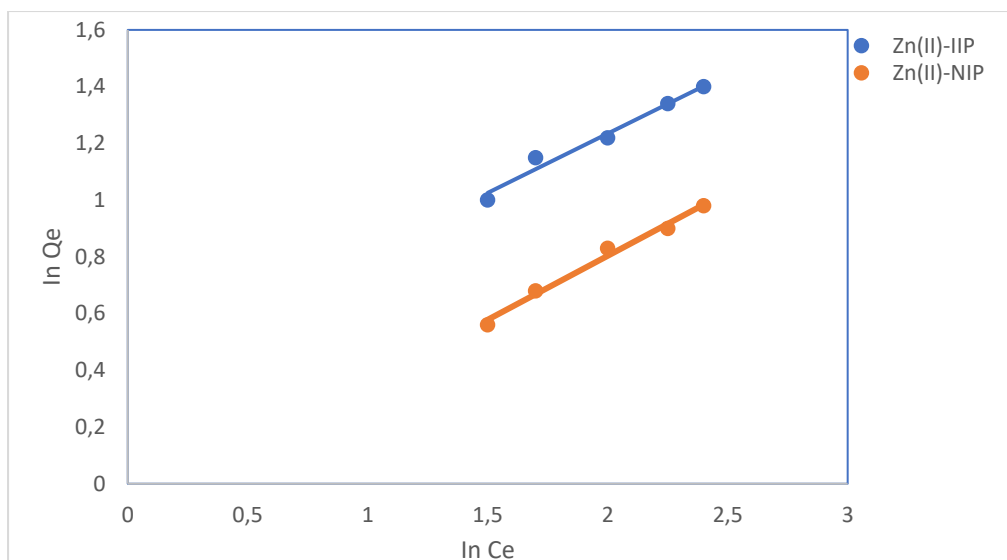


Figure 3.12: Temkin adsorption isotherm for adsorption of Zn (II) onto IIPs.

Table 3.5: Langmuir, Freundlich and Temkin values for the adsorption of Zn (II) on IIPs.

| Isotherm models | q_{max} | R_L | R² |
|------------------------------|------------------------|----------------------|----------------------|
| Langmuir isotherm | mg/g | | |
| | 9.03 | 0.45 | 0.99 |
| | B_T | K_T | R² |
| Temkin isotherm | J | L | |
| | mol ⁻¹ | mg ⁻¹ | |
| | 1.94 | 0.59 | 0.68 |
| Freundlich adsorption | 1/n | R _F | R ² |
| | 0.74 | 0.61 | 0.90 |

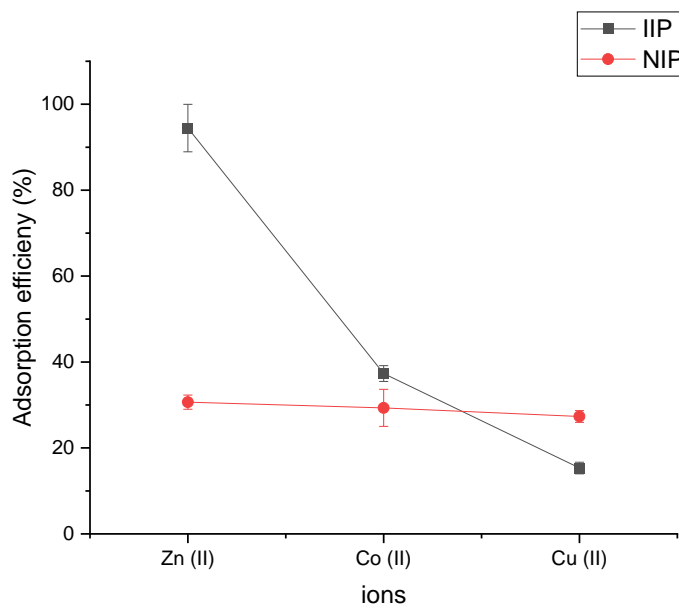
3.4.4. Selectivity studies

The selective adsorption of zinc ions co-occurring with competing ions like (Co (II)), (Pb (IV)), and (Cu (II)) was studied. These ions have similar ionic radii (Zn (II) = 74 pm, Co (II) = 74 pm, Pb (IV)= 79 and Cu (II) = 73 pm) and have the same charge. The zinc ion imprinted polymer (Zn-IIP) exhibited a higher adsorption efficiency of 90% in the presence of these competing ions, as shown in Table 3.6.

Table 3.6: K values of the NIP and IIP

| Adsorbent | K_d | | K | K' |
|------------|------------|-----------|-------|------|
| | Zn^{2+} | Cu^{2+} | | |
| IIP | 395.61 | 37.01 | 10.09 | 4.87 |
| NIP | 82.06 | 39.52 | 2.07 | |
| Adsorbent | Zn^{2+} | Co^{2+} | K | K' |
| | IIP | 1958.18 | | |
| NIP | 70.07 | 34.98 | 2.00 | 8.14 |

Figures 3.11 and 3.12 illustrate the adsorption efficiency of ions extracted by the IIP and NIP for individual ions and ion couples. The polymer demonstrated the ability to extract competing ions, as depicted in Figure 3.11. However, the highest selectivity was observed for Zn^{2+} ions, as the pores created in the polymer were specifically designed for zinc ions. Even in the presence of competing ions, the selectivity of the IIP for Zn^{2+} remained high. In contrast, the adsorption efficiency of the NIP was relatively low and comparable for all ions. This can be attributed to the absence of specific cavities in the non-imprinted polymer that would facilitate selective adsorption.


Figure 3.13: Adsorption efficiency for metal ions.

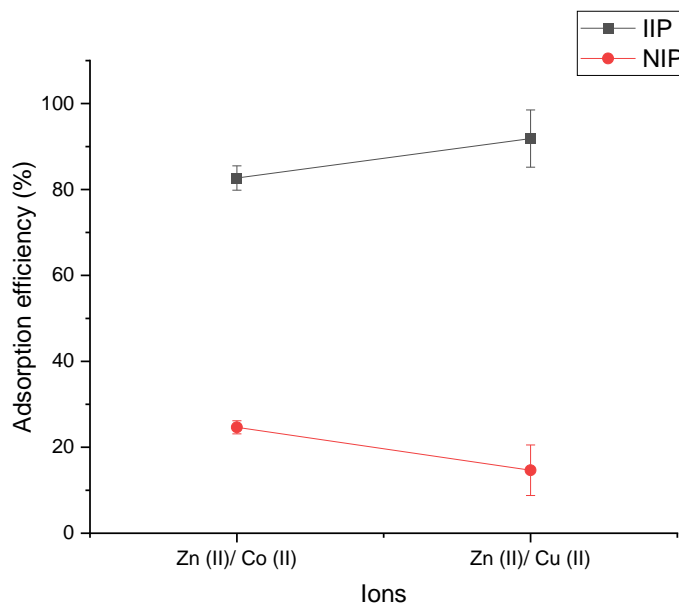


Figure 3.14: Adsorption efficiency in present of competing ions.

A competitive adsorption study was conducted in triplicate, involving species/ions with similar or comparable ionic radii that are commonly found alongside Zn (II). The distribution coefficient of the IIP was higher than that of the NIP, which is due to the selective binding sites present in the ion-imprinted polymer. Table 3.6 shows that the zinc ion-imprinted polymer exhibited greater selectivity towards Zn^{2+} compared to the other competing species. On the other hand, the non-imprinted polymer demonstrated similar affinity for all ions, as it lacked specific recognition sites for any ion.

3.5. Application of honey sample

The B vitamins: vitamin B6, folic acid, niacin, pantothenic acid, and riboflavin are all present in trace amounts in honey. Along with the minerals calcium, chromium, manganese, potassium, selenium, and others, it also contains ascorbic acid. The average concentration of zinc, potassium, magnesium, and copper in 100g of honey is 0.2–0.5 mg, 10–470 mg, 0.7–13 mg, and 0.01–0.1, respectively. According to Hungerford et al. (2020), trace element levels are generally low with the exception of zinc, iron, and manganese (Zn; 10.90 ± 24.7 mg/kg, Fe; 4.01 ± 6.98 mg/kg, and Mn; 4.48 ± 5.03 mg/kg), which are found at higher levels in honeys from rural areas compared to those from urban areas (Zn = 4.90 ± 11.17 mg/kg, Fe = 1.576 ± 1.33 mg/kg, and Mn = 2.385 ± 2.28 mg/kg). P (1.17–100.66), Fe (1.13–10.32), Al (0.02–13.04), Mn (0.07–0.68), Zn (0.14–3.87), Cu (0.05–0.68), Ca (18.60–136.14), Mg (6.01–46.57), Na (6.10–89.98), and K (90.92–1955.75) were the main trace elements in $\mu g g^{-1}$ of honey,

according to Khan et al. (2018). A honey sample was spiked with a known quantity of metal, and the recoveries were examined to evaluate the procedure. The technique detection limit and recovery outcomes for the detected elements are displayed in Table 3.7.

Table 3.7: Concentration of trace elements in honey.

| Metal ion | Concentration found in honey (mg kg⁻¹) | Concentration after spiking (mg kg⁻¹) | MDL(Method of detection limit) | Recovery % |
|------------------|--|---|---------------------------------------|-------------------|
| Cu | 1.05 | 1.92 | 0.0790 | 87.00 |
| Fe | 6.42 | 7.40 | 0.0159 | 98.00 |
| Ni | ND | 5.06 | 0.0253 | |
| Pb | 3.04 | 3.99 | 0.2531 | 95.00 |
| Mn | 4.95 | 6.59 | 0.0617 | 110.24 |
| Co | ND | 4.12 | 0.2251 | |
| Zn | 11.29 | 13.04 | 0.2431 | 99.00 |

ND = not detected

3.5.1. Determination of Zn(II) ions in honey samples

When the technique was used on actual honey samples, a high adsorption effectiveness of 94% was attained (Table 3.8). This proved that the sorbent was suitable for extracting zinc (II) ions from the honey sample in a selective manner.

Table 3.8: Removal of Zinc (II) from honey sample.

| Sample | Zn²⁺ spiked mg kg⁻¹ | RSD % | Zn²⁺ + IIP spiked mg kg⁻¹ | RSD % | AE % | RSD % |
|---------------------|--|--------------|--|--------------|-------------|--------------|
| Honey sample | 23.62 | 0.02 | 22.68 | 0.05 | 94.00 | 1.03 |

3.5.2. Comparative studies

A comparison of the adsorbent for removal of the zinc was done evaluating the adsorption efficiency as indicated in Table 3.9. Zinc ion imprinted polymer has higher adsorption efficiency than natural adsorbent.

Table 3.9: Comparison of adsorbent for removal of zinc (II).

| Adsorbent | Matrix | Adsorption capacity (%) | Reference |
|---|------------------|--------------------------------|-------------------------|
| Zinc ion imprinted polymer | Honey | 94.00 | This study |
| Oil palm empty fruit bunches biochar | Aqueous solution | 25.49 | Zamani et al. (2017) |
| Zinc oxide nano-material | wastewater | 95.00 | Primo et al., (2020) |
| Magnetic Chitosan | Aqueous solution | 83.81 | Karimi et al., (2022) |
| <i>Camellia sinensis</i> | Aqueous solution | 76.00 | Çelebi et al., (2020) |
| Natural bentonite | Aqueous solution | 90.00 | Esmail & Eslami (2019). |

3.6. Conclusion

Precipitation polymerization was used to create the zinc ion imprinted polymer, and the final polymer underwent extensive characterization. The cross-linking monomer was ethylene glycol dimethacrylate, and the initiator was 2,2'-azobis (isobutyronitrile), with methanol serving as the solvent. With the zinc ion-imprinted polymer (Zn-IIP), the maximum percentage of Zn²⁺ removed was about 90% when the following ideal parameters were met: a pH of 7.0 solution, 5 mg of adsorbent, 15 minutes of contact time, 100 rpm shaking rate, and a starting Zn²⁺ concentration of 25 mg/L. High adsorption capacity and superior selectivity for Zn(II) were displayed by the Zn-IIP, allowing it to keep out competing ions such as Cd (II), Pb (II), and Cu (II). The adsorption of Zn (II) onto Zn-IIP was characterized by pseudo-second-order kinetics. Additionally, utilizing the Zn-IIP to remove zinc showed an amazing adsorption capacity of 98%.

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Chapter 4: Synthesis of lead-ion imprinted polymers for selective extraction of Pb (II) from wastewater

Abstract

Synthesis of IIP and NIP for selective extraction of Pb (II) ions from wastewater was attempted. Precipitation copolymerization of methacrylic acid as the monomer, ethylene glycol dimethacrylate as the cross-linker, and 2,2'-azobis (isobutyronitrile) as the initiator was used to create IIPs and NIPs. After leaching the template ion out of the IIPs with 2 M hydrochloric acid, cavities in the polymer matrix formed that could selectively complex Pb (II) ions. FTIR was used to characterize the functional groups of the imprinted and non-imprinted polymers, and the ideal parameters of 50 mg of adsorbent, pH 9 of the starting solution, and 15 minutes of contact time were used to determine the point of zero charge. The IIP and NIP's adsorptive qualities were assessed using Freundlich and Langmuir isotherms. The data was better modeled by the Langmuir adsorption isotherm, as indicated by the 0.999 and 0.975 Langmuir and Freundlich correlation coefficients, respectively. The adsorption occurred on homogenous surfaces. Lead can potentially be recovered from waste water using the imprinted polymer.

Keywords: Ion imprinted polymer, thiosemicarbazide, lead (II) ion, precipitation polymerization and selective removal.

4.1. Introduction

Our society's industrial development results in significant emissions of pollutants and trace elements. In the food chain, trace elements build up. When they reach the body, they mix with inorganic substances to form complexes that are harmful to the body because they cannot break down or be expelled (Emenike et al., 2021; Sonone et al., 2020; Tang et al., 2021). One prevalent trace element that contaminates the environment is lead. Wastewater from paints, lead-acid batteries, phosphate fertilizers, and lead corrosion are its sources. Lead exposure over time can cause memory loss and low IQ.

It has been discovered that some of the trace elements in wastewater are beyond the maximum permitted limits and coexist with other competing species rather than existing alone. Owing to these reasons, a more effective technique for eliminating trace elements from native solutions had to be created (Dimpe and Nomngongo, 2017). A few of the techniques created are osmosis, liquid-liquid extraction, and membrane assisted liquid extraction (Golcs et al., 2021; Tabani et al., 2018; Ding et al., 2021). Lead may be extracted from solutions with great efficiency using adsorption techniques (Zhao et al., 2016; Zare-Dorabei et al., 2016).

Pb^{2+} removal from various solutions has been investigated for the effectiveness of a number of adsorbents, including zeolite, metal oxides (ZnO , TiO_2 , and iron oxide), activated carbon, and both synthetic and natural polymers (β -cyclodextrin) (Shah et al., 2017; Genç and Dogan, 2015). High activation costs and inadequate recycling restrict the use of activated carbon, despite its excellent adsorption efficiency towards Pb^{2+} (Lin et al., 2020; Lin et al., 2023; Zhanga et al., 2019; Zhao et al., 2020). Zeolites are highly susceptible to irreversible adsorption-induced deactivation (Hu et al., 2022; Luo et al., 2022; Li et al., 2023). Metal oxides are extremely sensitive to grinding conditions and can be impacted by unintentional contamination from the environment and milling media. Low cost, physical stability, porosity, homogeneous pore size distribution, and ease of regeneration characterize polymeric adsorbents. Regeneration can lessen the need for new adsorbent, which is crucial from an economic and environmental standpoint, as well as the need to dispose of spent adsorbent. According to Hassan et al. (2020) and Janoschka et al. (2015), they can operate across a wide pH range.

In the presence of closely related inorganic ions, ion-imprinted polymers are non-porous polymeric materials that, upon leaching the imprint ion, can rebind, detect, or transport the target analyte selectively (Abdallah et al., 2021; Stevens and Batlokwa, 2017; Pereo et al., 2018). Ion-imprinted polymers are distinguished by their extended shelf life, strong affinity, and target ion selectivity. When a template ion and a functional monomer are combined, the monomer self-assembles around the template. A cross-linker will be added for the polymerization process to proceed. Using an appropriate extraction porogen that leaves the memory site or binding site complimentary to a certain template, the template is eliminated following polymerization. In the solid phase, ion-imprinted polymers are used for preconcentrating, ion removal, and separation ion from coexisting ions (Xie et al., 2019; Omidi et al., 2014). According to Balouch et al. (2014) more than 96% of Pb could be recovered from real samples, and grafted-IIP retained more than 80.5% adsorption capacity (Wang et al., 2019).

Thiosemicarbazide ($\text{NH}_2\text{NH}-(\text{C}=\text{S})=\text{NH}_2$) is a hydrazine derivative of thiocarbamic acid that is commonly used in organic synthesis of heterocyclic compounds such as pyrazoles, thiazole and triazines (Karrouchi et al., 2018). Thiosemicarbazide derivatives are used in catalysis, electrochemistry and pharmaceutical chemistry, under catalysis for redox reaction is used for antitumor, antimalarial agent, antibacterial and electrochemical sensors (Hishimone et al., 2021). Thiosemicarbazide has been used also in industry for applications like anti-corrosion

and anti-fouling effects have also been reported for these derivatives (Acharya et al., 2021 & Kanwar et al., 2015). It is a bidentate ligand which is coordinated with transition metal. It forms complexes with different cations such as zinc, iron, nickel, copper and others (Muleta et al., 2019).

In this work, a Pb (II) IIP and a NIP were produced by precipitation polymerization due to the good yield and shorter time needed compared to bulk polymerization where there is grinding and sieving. Polymers were complexed with thiosemicarbazide before applied for selective extraction of Pb ion from aqueous solution. Pb-IIPs were characterized by FTIR and point of zero charge followed by solid phase extraction of a target metal ion extracted from the wastewater onto the IIPs absorbed into the IIPs by different techniques and to determine trace elements in the wastewater.

4.2. Materials and methods

4.2.1. Chemicals and reagents

All chemicals and reagents including, methanol (CH₃OH) (99.85%) grade A, methacrylic acid (C₅H₈O₂) (MAA) (99.5%) grade A, azobisisobutyronitrile (C₈H₁₂N₄) (AIBN) (98%) A, ethylene glycol dimethacrylate (C₁₀H₁₄O₄) (EGDMA) (99%), lead acetate trihydrate (C₄H₁₂O₇Pb) (99.99%) ACS, hydrochloric acid (HCl) (37%) AR, zinc sulphate (ZnSO₄) (99%) AR and thiosemicarbazide (CH₅N₃S) 98% AR were sourced from Merck (Wadesville, South Africa). Cobalt (II) chloride (CoCl₂) (97%) LR and copper (II) sulphate (CuSO₄) (98%) LR were bought from Sigma-Aldrich (Johannesburg, South Africa).

4.2.2. Instrumentation

Infrared spectroscopy was implemented to differentiate the IIP functional groups before and after extraction and non-imprinted polymer (Pretoria, South Africa). The concentration of metal ions in samples was measured by Pb²⁺ ion analysis using atomic absorption spectroscopy (Pretoria, South Africa).

4.2.3. Synthesis of Pb²⁺ ion imprinted polymers (IIPs)

The modified method of Xia et al. (2017) was used to prepare Pb²⁺ IIP and NIP. The Pb(C₂H₃O₂)₂·2H₂O template (0.116 g) and 422 μL (5 mmol) C₄H₆O₂ were added to 70 mL methanol in a 250 mL one-neck round-bottomed flask. After stirring for 15 min to homogenize the solution it was purged to remove oxygen and provide an inert atmosphere before adding 2 mL (10 mmol) C₁₀H₁₄O₄. After 2 min purging of the mixture with nitrogen to displace oxygen, the C₈H₁₂N₄ initiator (50 mg) was added. The flask was greased, loosely closed with lead and

covered with parafilm. The flask was then heated for 7 h at 80°C in an oil bath. After filtration, the product was collected and allowed to dry overnight. The NIPs were prepared using the same process without a template.

4.2.4. Elution of Pb²⁺ IIP

After polymerization of the IIPs and non-imprinted polymer, they were rinsed eight times with 2 M HCl to extract the template (Tavengwa et al., 2016), as shown in Figure 4.1. The obtained IIPs and NIPs (3 g and 1 g, respectively) were transferred to 50-mL solid phase cartridges with a cotton wool plug on the bottom. The elution process was done in continuous mode. The eluted was collected after every hour. The procedure was repeated eight times for both IIPs and NIPs. The wet IIPs and NIPs were dried for overnight.

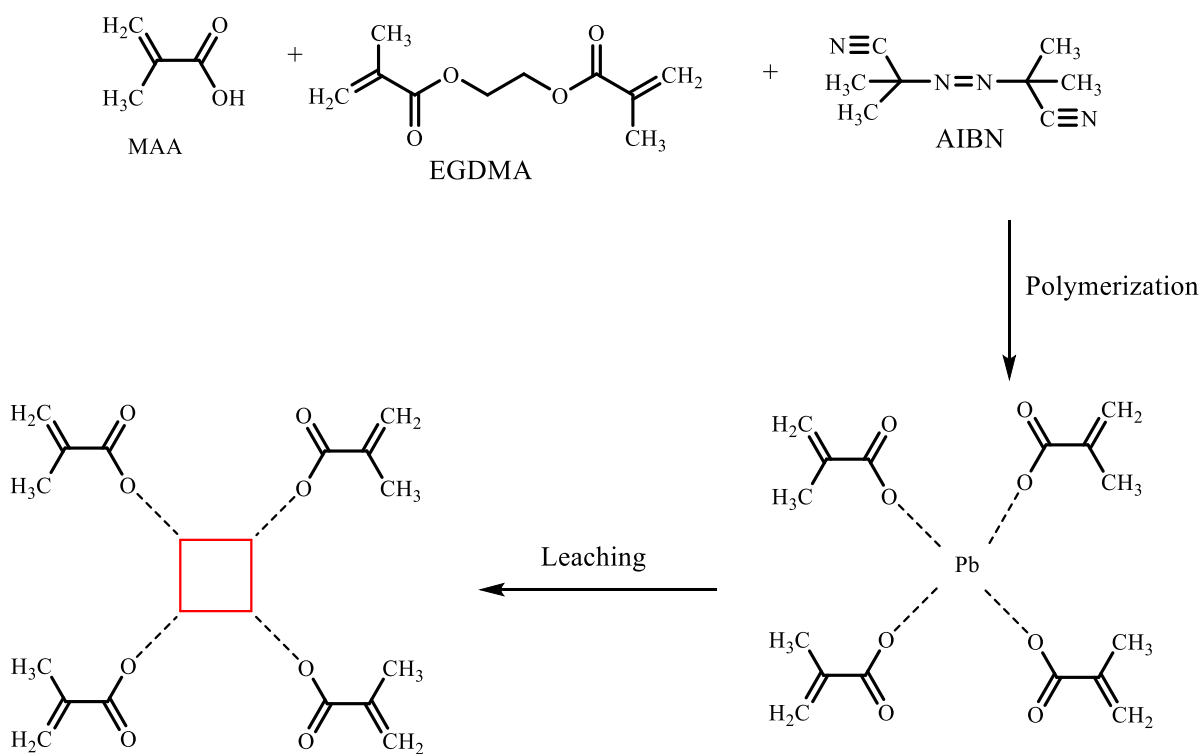


Figure 4.1: Scheme illustrating imprinting process for Pb (II) imprinted polymer.

4.2.5. Batch experiment

In a batch experiment to adsorb Pb²⁺ from aqueous solution, one parameter was investigated while keeping others constant. The parameters investigated include sample pH, dosage, contact time and concentration. Lead ion imprinted polymer of 30 mg was suspended into a Pb²⁺ solution of 5 mg/L. Sample pH was adjusted by dropwise addition of 0.1 M HCl or NaOH. Using a shaker and a centrifuge (NF 1200; PROG No. 7, RPM/RCF 4010, Time 5 min, and

ACC/BRK 5), the mixtures were agitated at 75 rpm for 20 minutes and filtered with Whatman filter papers (150 μm) for analysis with UV-VS spectrometry after being mixed with complexing agent thiosemicarbazide with a 1:3, v/v solution. The purpose of adding complexing was for Pb-IIP and Pb-NIP to be active in UV-VS. According to Bharty et al. (2019), thiosemicarbazide is commonly ligand for transitional metals. The metal complex occurs through S atom. The spectra were recorded for each sample on SP8001 spectrophotometer wavelength at the range 200-800 nm with a cuvette of 1 cm path length. The percentage adsorption E and adsorption capacity Q_e (mg g^{-1}) were computed as follows:

$$E = \frac{C_i - C_f}{C_i} \times 100 \quad (4.1)$$

$$Q_e = \frac{(C_i - C_f) V}{W} \quad (4.2)$$

where C_i and C_f = initial and final concentrations (mg L^{-1}) of Pb (II), respectively,

W = sorbent weight (g), and

V = solution volume (mL).

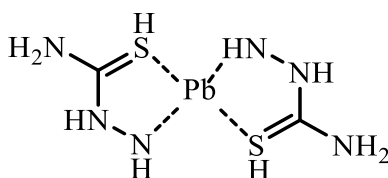


Figure 4. 2: Structure of Pb (II)- thiosemicarbazide

4.2.6. Adsorption isotherms

Over the range of 10-45 mg/L of Pb^{2+} concentration, adsorption isotherms were assessed. Pb^{2+} -IIP and Pb^{2+} -NIP (50 mg) were added to the solution after it had been brought to pH 7 with 0.1 M NaOH or HCl. After shaking the mixture for one hour at room temperature, the polymers were gathered by filtering, and UV-VIS spectroscopy was used to determine the Pb^{2+} content.

The Langmuir and Freundlich adsorption isotherms were found using the adsorption data. According to the Langmuir adsorption isotherm model, homogeneous sites are the locations of adsorption on the adsorbent's surface, and once a molecule is absorbed onto a site, it prevents other molecules from absorbing there (Buelvaj et al., 2023; Gohari et al., 2022; Kumar et al., 2019; Mohammadi et al., 2019 and Zou et al., 2023).

Langmuir equation can be expressed as

$$\frac{C_e}{q_e} = \frac{1}{q_{\max}b} + \frac{C_e}{q_{e \max}} \quad (4.3)$$

where q_e = equilibrium amount of adsorbate (mg g^{-1})

C_e = ion concentration in the solution

q_{\max} = maximum sorption capacity

b = Langmuir constant

The Freundlich adsorption isotherm, on the other hand, works with heterogeneous surfaces. According to Ayawei et al. (2015), it specifies surface heterogeneity and the exponential distribution of activation energies.

$$\log q_e = \log R_F + \frac{1}{n} \log C_e \quad (4.4)$$

where R_F = adsorption capacity (L/mg), and

$1/n$ = adsorption intensity; it also indicates the relative energy distribution and the heterogeneity of the adsorbate sites.

4.2.7. Selectivity studies

The selectivity study was conducted under optimized conditions for the IIP and the NIP. The IIP or NIP (50 mg) was added to a 10 mL aqueous solution containing $0.1 \mu\text{g mL}^{-1}$ each of Co (II), Cu (II) and Ni (II). These competing ions were chosen due to their identical charge, comparable ionic radii, and frequent coexistence with Pb^{2+} ions.

The sample pH was adjusted to 9 using 0.1 M HCl or NaOH. The mixture was placed in a 15 mL centrifuge vial and stirred at 70 rpm for 15 min. The experiment was performed in triplicate. The mixture was then filtered, and thiocarbazine was complexed with the filtrate. Using AAS, the ion concentrations were determined. Eqs. 4.5–4.7 were used to calculate the distribution ratio (K_d), selectivity factor (K), and relative selectivity factor (K') of Pb (II) in relation to Co (II), Cu (II), and Ni (II):

$$K_d = \frac{(C_i - C_f)V}{C_fM} \quad (4.5)$$

$$K = \frac{K_{d(\text{Pb(II)})}}{K_{d(\text{competing ions})}} \quad (4.6)$$

$$K' = \frac{K_{\text{imprinted}}}{K_{\text{non-imprinted}}} \quad (4.7)$$

4.2.8 Reusability studies

When used industrially, adsorbent regeneration plays a crucial role. In this study, polymers were loaded and leached several times by adding 50 mg of polymer to 20 mL of 35 mg/L Pb (II) in deionised water. The Pb(II) was leached with 20 mL 2 M HCl in continuous mode.

4.2.9. Real sample

4.2.9.1. Wastewater sampling preparation

The wastewater was collected from Limpopo Tswinga Water Waste Treatment Plant. Three samples were collected in outlet, biofilter and final and the physico-chemical properties were recorded in Table 1. All samples were acidified with nitric acid and keep it at 4 °C.

Table 4.1: Determination of metal ions in water.

| Metal ion | Concentration Found (mg.kg⁻¹) | Concentration after spiked (mg.kg⁻¹) | Amount spiked (mg.kg⁻¹) | Recovery (%) | MDL |
|------------------|---|--|---|---------------------|------------|
| Pb | 3.20 | 3.48 | 0.30 | 99.98 | 0.01 |
| Cu | 1.56 | 1.87 | 0.30 | 90.00 | 0.02 |
| Fe | 4.50 | 4.79 | 0.30 | 96.97 | 0.08 |
| Zn | 1.10 | 1.39 | 0.30 | 96.67 | 0.12 |
| Cr | 1.80 | 2.11 | 0.30 | 99.68 | 0.19 |

Table 4.2 shows the properties of wastewater from different place in in treatment plant which include the outlet, biofilter and final.

Table 4.2: Physico-chemical properties of wastewater.

| | | |
|-----------|---------------------------|----------|
| Outlet | TDS (mg L ⁻¹) | 270 |
| | Temperature (°C) | 25.00 °C |
| | EC (µ/s) | 447 |
| | Ph | 7.50 |
| Biofilter | TDS (mg L ⁻¹) | 286 |
| | Temperature (°C) | 25.8 |
| | EC (µ/s) | 445 |
| | Ph | 7.60 |
| Final | TDS (mg L ⁻¹) | 286 |
| | Temperature (°C) | 24.8 |
| | EC (µ/s) | 445 |
| | Ph | 7.60 |

4.2.9.2. Digestion of wastewater samples

The modified method of Ambuse et al. (2020) was applied to digest the wastewater samples. The wastewater was shaken thoroughly and filtered. It was digested in 3 mL concentrated HNO₃ and 3 mL H₂O₂ at 80°C for 1 h until it was clear. The clear solution was diluted to 100 mL volumetric flask and the selected heavy metals were detected using AAS as indicated in Table 4.3. The metals that were determined were Cu, Zn, Fe and Mn as are the competitors of Pb. These metals have the same charges and are commonly found in wastewater (Qusem et al., 2021).

Table 4.3: Parameters of AA determination of heavy metals.

| Parameters | Cu | Fe | Zn | Pb | Mn |
|-----------------|--------|--------|--------|--------|--------|
| Wavelength (nm) | 324.75 | 248.33 | 307.59 | 283.31 | 279.48 |

| | | | | | |
|---------------------|-----------|-----------|-----------|-----------|-----------|
| Current (mA) | 15 | 30 | 14 | 10 | 20 |
| Slit (nm) | 0.7 | 0.2 | 0.7 | 0.7 | 0.2 |
| Lamp type | C- HCL | C- HCL | C- HCL | C- HCL | C- HCL |
| Energy | 88 | 62 | 40 | 82 | 70 |

4.3. Results and discussion

4.3.1. Functional groups characterization of lead imprinted polymer by FTIR

The FTIR spectra depicting the functional groups of IIP leached, IIP un-leached and NIP are represented in Figure 4.3. Transmittance peak in the region 3424 cm^{-1} is present in leached IIP, un-leached IIP and absent in the NIP since it shows the absorption of OH. This band frequency at 3424 cm^{-1} is broad, strong and sharp in washed IIP compared to unwashed IIP. Vibration absorption at about 1716 cm^{-1} appeared in both IIP and NIP polymer which shows the present of C=O bond, other band it is at 2951 cm^{-1} which shows the present of C-H in both polymers. There is a present of a peak in 1256 cm^{-1} and 1146 cm^{-1} in both polymer which confirm the present of C=C and C-O respectively. At a region of about 466 cm^{-1} , it shows the Pb-O present in unwashed IIP and NIP while in washed IIP its absent since it was eluted. The absence of vinyl groups in polymer materials was evident from the clear lack of an absorption band in the $1648\text{--}1638\text{ cm}^{-1}$ range, confirming the full polymerization of methacrylic acid.

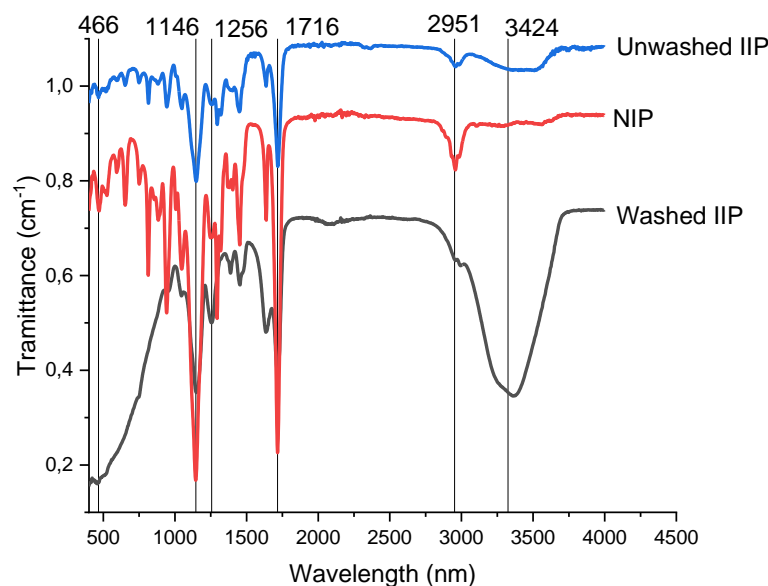


Figure 4.3: Infrared spectra of Pb (II) ion imprinted polymer/NIP.

4.3.2. Effect of sample pH

The impact of solution pH on lead adsorption efficiency is shown in Figure 4.4. The resulting data shows that below pH 2.0, the adsorption efficiency for Pb (II) ions is abnormally low. pH 9.0 was shown to be the ideal pH for optimal adsorption effectiveness. For the Pb (II) ion, an increase in adsorption effectiveness was solution pH increased from 3 to 9.0. The adsorption capabilities of Pb (II) IIP and NIP decreased at solution pH values greater than 9.0. This makes sense because as the pH of the solution drops, the polymer's surface becomes protonated, which acts as a repellent to the metal cations and prevents them from approaching. Conversely, as the pH of the solution rises, some of the functional groups begin to separate, becoming negatively charged and drawing the metal cations in. This theory is supported by the pHZPC values of Pb(II)-IIP and Pb(II)-NIP, which show that the surface became negatively charged above pH 6.0, allowing Pb^{2+} metal cations to more easily migrate to the negatively charged IIP surface. However, because $Pb(OH)_2$ is produced more frequently above pH 9 and these species have poor adsorption capabilities, the amount of adsorption reduced.

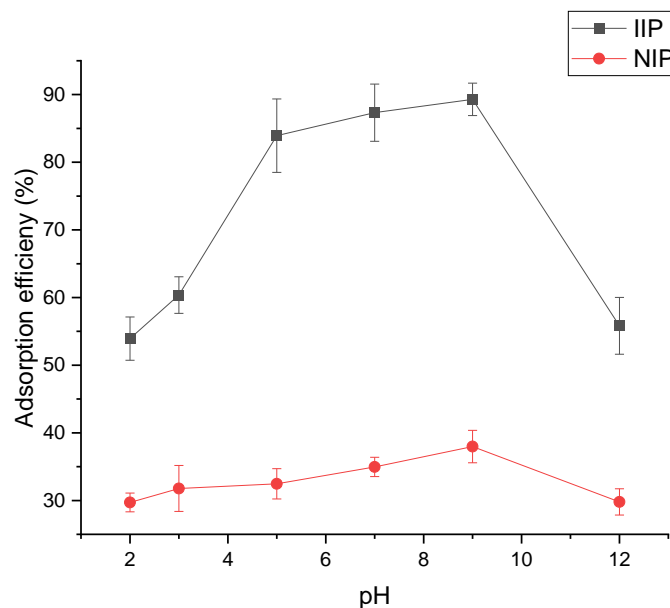


Figure 4.4: Effect of solution pH on Pb(II) adsorption. Conditions: adsorbent mass = 50 mg, initial concentration = 0.5 mg/L, contact time = 20 min, and shaking speed = 70 rpm at room temperature.

Finding the sorbent's point of zero charge (pHPZC) is necessary to understand the adsorption process. When the pH of the solution is less than pHPZC, anion adsorption efficiency is more advantageous than cation adsorption efficiency. The pHPZC is shifted to lower values by specific cation adsorption and to higher values by specific anion adsorption. Stated differently, the pH point of zero pHPZC is the pH value that, in the absence of particular sorption, results in a net zero charge on the solid polymer surface. When the charge on the polymer surface varies from zero as a function of solution pH, this happens. Plotting the Pb (II) IIP's recorded positive and negative pH changes against the pH of the starting solution, pH_i, yields the pHPZC at the pH value where ΔpH equals 0. It was discovered that Pb-IIP and Pb-NIP both have a point of zero charge of 6. The cation adsorption is favoured by the implemented $\text{pH} > \text{pHPZC}$.

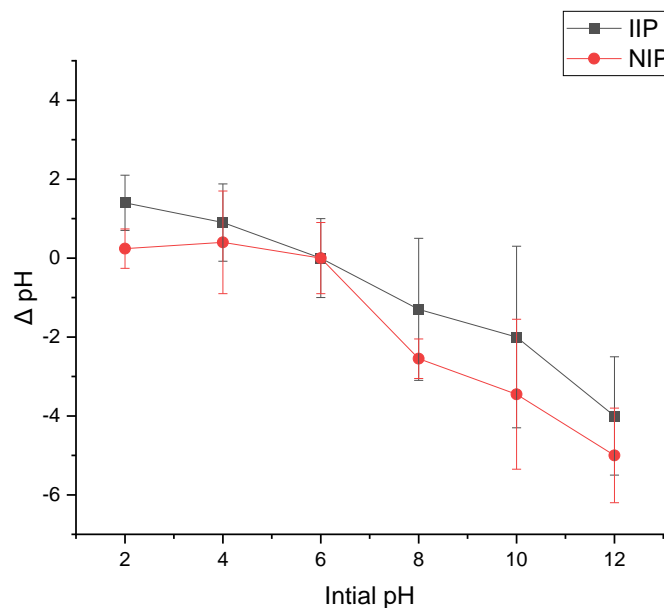


Figure 4.5: Point of zero charge Pb (II). Experimental conditions: 50 mg, shaking speed 70 rpm for 15h.

4.3.3. Adsorbent dosage

The amount of adsorbent, which was investigated in the range of 10-70 mg/100 mL, is significant. Up to 50 mg of ion-imprinted polymer, the Pb (II) removal efficiency increased with increasing adsorbent loading (Figure 4.6). The quantity of adsorption sites that are available may be the cause of this rise in adsorption effectiveness. Nevertheless, the concentration of metal ions achieved equilibrium, therefore adding more imprinted polymer did not result in any additional increase in adsorption. The imprinting effect is responsible for the Pb(II)-IIP's superior extraction efficiency (> 89.31%) by 50 mg polymer material as opposed to NIP's (> 38.13%).

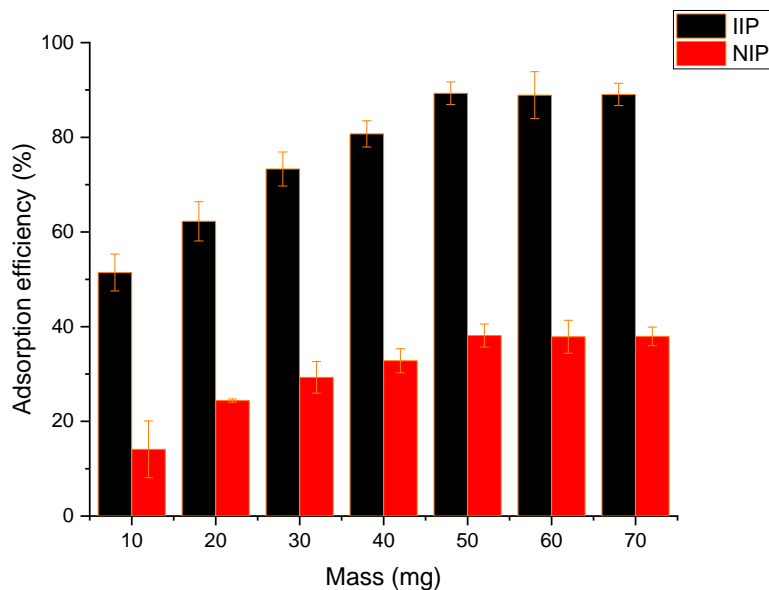


Figure 4.6: Influence of adsorbent mass on Pb (II) adsorption (n = 3, SD). Conditions: pH = 9, sample volume = 10 mL, initial concentration = 0.5 mg/L, contact time = 20 min, shaking speed = 70 rpm at room temperature.

4.3.4. Effect of time

Using both Pb(II)-IIP and NIP particles, the effect of agitation time on the adsorption of Pb²⁺ ions from aqueous solutions was investigated. As seen in Figure 4.7, the adsorption process began with rising adsorption rates and eliminated 85% of Pb (II) after 15 minutes. 15 minutes passed with no more adsorption.

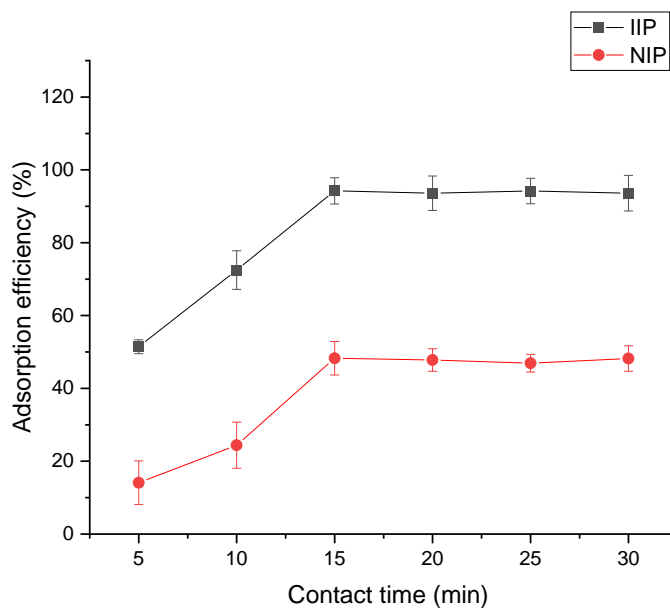


Figure 4.7: Influence of contact time on Pb(II) adsorption ($n = 3$, SD). Conditions: adsorbent mass = 50 mg/L, sample pH = 9, sample volume = 10 mL, and shaking speed = 70 rpm at room temperature.

4.3.5. Concentration effect

Figure 4.8 illustrates how adsorption changes with ion concentration. There was a range in Pb(II) concentration from 10 to 45 mg/L. As the Pb(II) concentration rose from 10 to 35 mg/L, the adsorption effectiveness increased while maintaining the same duration, pH, and IIP dosage. The saturation of sites caused the adsorption to become constant. Pb-IIP has more adsorption sites than Pb-NIP, as evidenced by the fact that its adsorption efficiency is higher than Pb-NIP's.

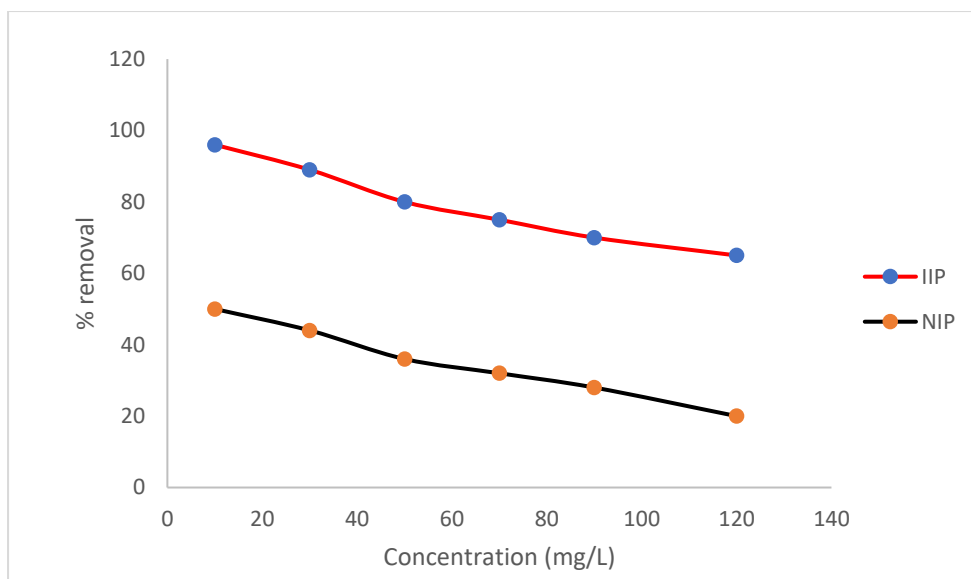


Figure 4.8: Influence of initial Pb(II) ion concentration on adsorption efficiency (n = 3, SD).
Conditions: Sample pH = 9, mass = 50 mg, sample volume = 10 mL, temperature = 313 K,
shaking speed = 70 rpm and time = 15 min.

Figures 4.9(a) and (b) exhibit the Langmuir and Freundlich adsorption isotherms for Pb²⁺ adsorption onto NIP and IIP, and Table 4.3 displays the constants that were determined. For the Pb (II)-IIP and Pb (II)-NIP, the correlation coefficients (R_2) of the Langmuir and Freundlich adsorption isotherms were determined to be, respectively, 0.999 and 0.991 and 0.975 and 0.965. As a result, the Langmuir adsorption isotherm, which suggests monolayer adsorption, best describes the Pb (II) adsorption by the IIP and NIP. During the adsorption process, the adsorbate ion covers the adsorption site. This notion is predicated on a uniform surface of pores. Pb(II) IIP and Pb (II)-NIP were reported to have maximal adsorption capacities of 54.40 and 12.01 mg g⁻¹, respectively. Furthermore, given that $n > 1$, the Freundlich model suggests that adsorption occurs more easily on Pb (II)-IIP surfaces due to the affinity between Pb (II) ions and Pb (II)-IIP.

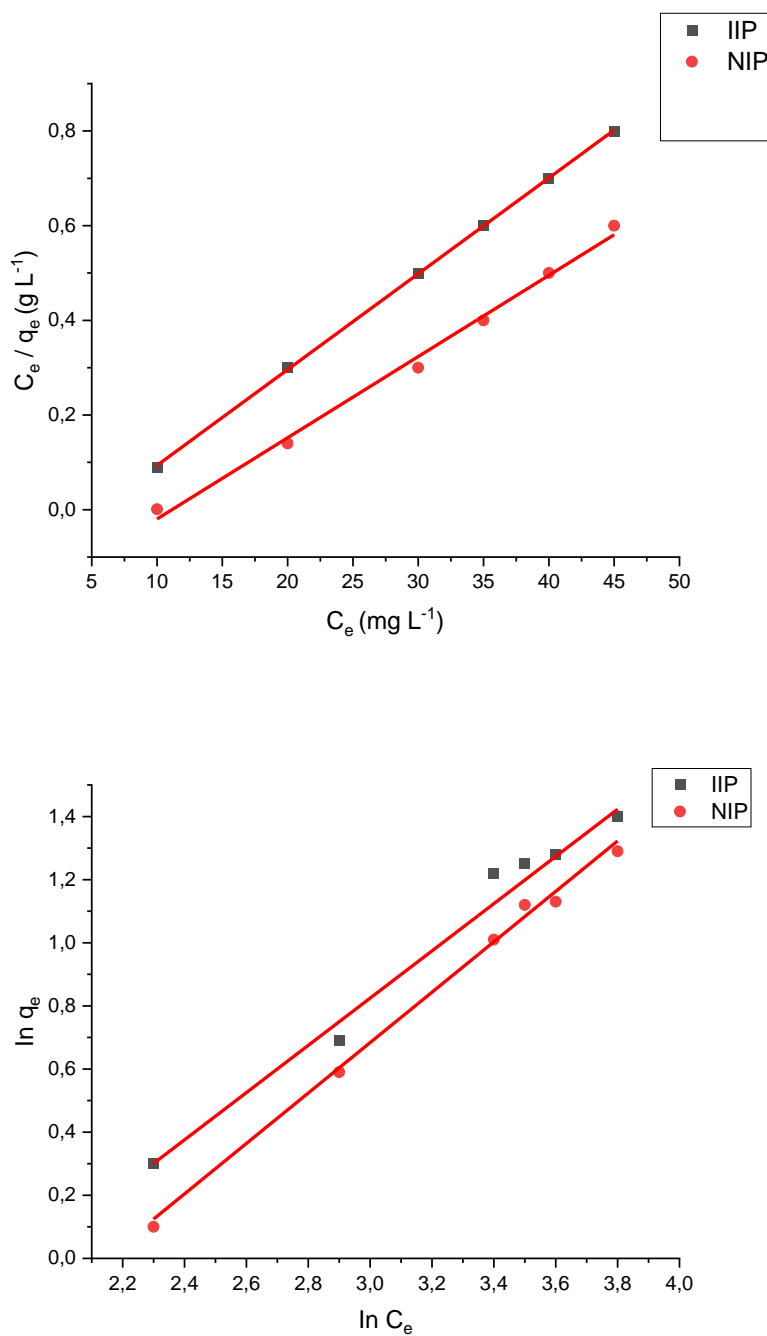


Figure 4.9: Langmuir (a) and Freundlich (b) adsorption isotherm of lead ion on the lead ion imprinted polymer. Conditions: Adsorbent dose = 50 mg, solution pH = 9 and adsorption time 3 h at room temperature.

Table 4.4: Langmuir and Freundlich isotherms

| Langmuir and Freundlich adsorption isotherms | | | | | | |
|--|--------------------|--------------------|-------|------------|------|-------|
| Adsorbent | Langmuir | | | Freundlich | | |
| | $q_{e\text{ cal}}$ | $q_{e\text{ exp}}$ | R^2 | K_f | n | R^2 |
| Pb (II)- IIP | 60.54 | 58.4 | 0.999 | 38.40 | 3.28 | 0.975 |
| Pb (II)- NIP | 12.45 | 12.01 | 0.991 | 30.01 | 5.67 | 0.965 |

4.3.6. Selectivity studies

The above mentioned work shows that the Pb (II) imprinted polymer has suitable sites for the target ion, with the right cavity size, thus increasing the selectivity. It shows that the Pb (II)-IIP can recognize specifically Pb (II) ions, due to the size and morphology of the cavities imprinted in the polymer. The Pb²⁺ IIP selectivity coefficients (K) versus Co²⁺, Cu²⁺ and Ni²⁺ were found to be 94.67, 43.55, and 177.75, respectively, as shown in Table 4.5. The selectivity of IIP was always higher than the selectivity of NIP, as presented in Figures 4.10 and 4.11. The IIP has a high selectivity due to the monomer that provides specific binding sites for the target ion.

Table 4.5: Selectivity study of Pb (II) ion imprinted polymer.

| Metal ion | Non-imprinted polymer | | Ion imprinted polymer | | |
|------------------|-----------------------|-------|-----------------------|--------|------|
| | K_d | K | K_d | K | K' |
| Pb ²⁺ | 1.19 | | 8.71 | | |
| Co ²⁺ | 0.09 | 13.37 | 0.09 | 94.67 | 7.08 |
| Cu ²⁺ | 0.14 | 8.32 | 0.20 | 43.55 | 5.23 |
| Ni ²⁺ | 0.06 | 20.16 | 0.05 | 177.75 | 8.82 |

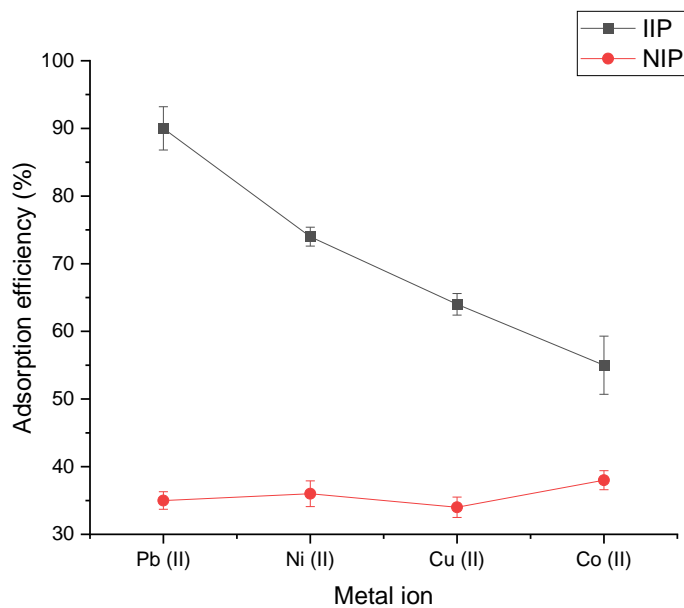


Figure 4.10: Adsorption efficiency for metal ions.

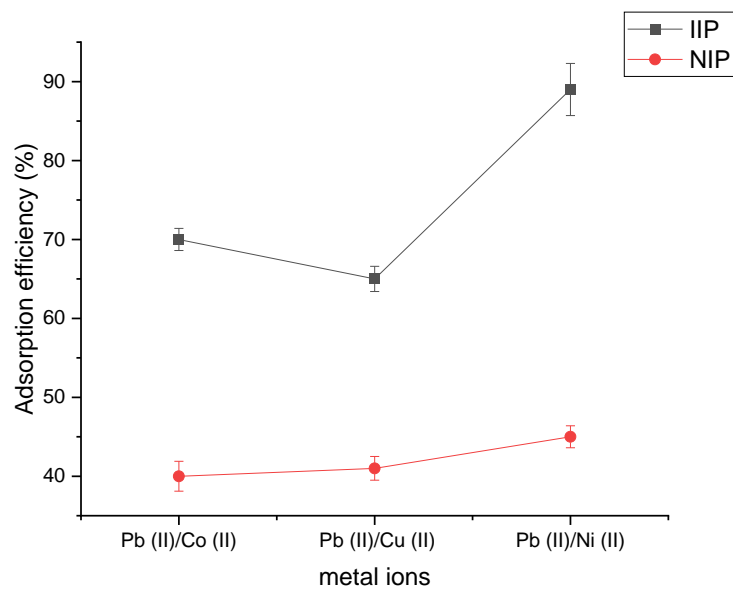


Figure 4.11: Adsorption efficiency in the presence of competing ions.

4.3.7 Removal of Pb (II) from wastewater.

Three samples were collected at Tswinga, where the outlets have higher concentrations followed by biofilter and final samples. Lead ion imprinted polymer show a high adsorption efficiency above 90% for all samples, as indicated in Table 4.6.

Table 4.6: Removal of Pb (II) from wastewater samples, n = 3.

| Sample | Pb ²⁺ spiked | RSD % | Pb ²⁺ + IIP spiked | RSD % | AE % | RSD % |
|-----------|----------------------------|----------|-------------------------------------|----------|---------|----------|
| Outlets | 3.48 | 0.02 | 2.55 | 0.05 | 93.00 | 1.03 |
| Biofilter | 3.00 | 0.01 | 2.03 | 0.03 | 97.00 | 0.05 |
| Final | 2.60 | 0.09 | 1.66 | 1.02 | 94.00 | 0.09 |

Percentage removal of Pb (II) from wastewater with Pb (II) IIP as adsorbent was higher than when using a lead ion imprinted interaction polymer network, as shown in Table 4.7.

4.3.8. Comparison studies

The removal efficiency of the Pb (II) ion imprinted interpenetrating polymer network was lower, which may have been caused by the complexing monomer chitosan, the porogen used which was toluene, and the crosslinking agent which was tetraethyl-orthosilicate (TEOS).

Table 4.7: Comparative study for removal of Pb (II).

| Sorbent | Extraction of Pb (%) | Sample | Reference |
|--|-------------------------|------------|-------------------------|
| Lead ion imprinted interpenetrating polymer network | 91.5 | Wastewater | Hande et al., (2016) |

| | | | |
|------------------------------|------|------------|------------------------------------|
| Activated carbon | 98.0 | Water | Lakshmikandhan and Ramadevi (2019) |
| Ion imprinted polymer | 95 % | Wastewater | This study |

4.3.9. Reusability studies

The ability to reuse an adsorbent is crucial in evaluating the IIP efficiency and to develop applications that are reliable, economic and sustainable. Ion imprinted polymers are stable and reusability they can perform over 100 adsorption regeneration cycles (Kupai et al., 2017). Chain length affects both flexibility and strength (longer chains equal greater strength), side groups polar side groups increase the attraction between polymer chains, strengthening the polymer and cross-linking polymer chains are joined by covalent bonds, which harden and complicate the melting of the polymer. These properties allow these polymers to be generated and reused. Because hydrochloric acid increases pore diameter, it facilitates easier absorption and desorption. Figure 4.12 shows that there is very little decline in adsorption after the same polymer is used seven times.

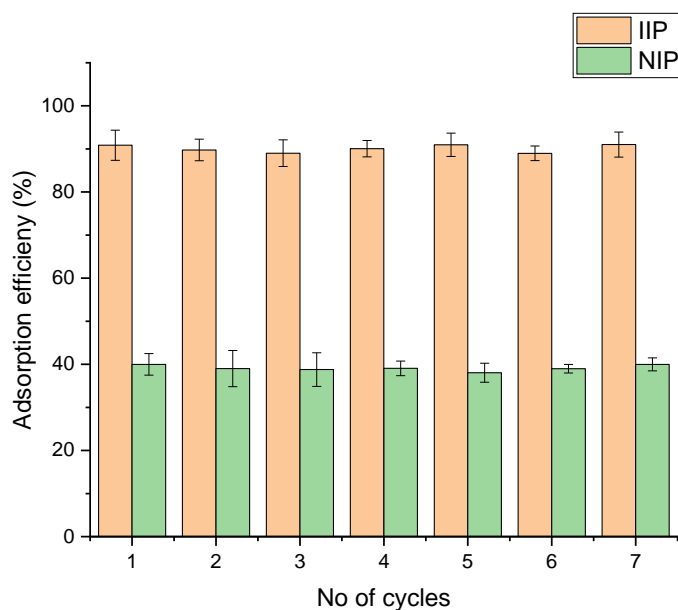


Figure 4.12: Reusability study of Pb (II) ion imprinted polymer.

4.4. Conclusion

Precipitation polymerization was used to create a lead (II) IIP. Using infrared spectroscopy, the functional groups of the lead IIP and NIP were identified. The maximum adsorption efficiency was achieved under the following conditions: sample pH = 9, adsorbent mass = 50 mg, Pb(II) concentration = 35 mg/L, and contact time = 15 min. The adsorption efficiency was examined in batches for various parameters. The Langmuir isotherm promoted Pb(II) adsorption on Pb (II) ion imprinted polymers. The Pb (II) IIP's selectivity was demonstrated by the increased Pb (II) removal in the selectivity research, with a selectivity coefficient above 40. Three authentic samples were gathered, and the concentrations of heavy metals found were $Fe > Pb > Cr > Cu > Zn$. It was shown that Pb (II) IIP removed more than 90% of Pb (II) from wastewater. Additionally, the reusability study was assessed seven times, and the high adsorption effectiveness of 90% indicated that the waste material would be useful for future use in this investigation.

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Chapter 5: Conclusions and recommendations

5.1 Conclusions

Ion imprinted polymers were successfully synthesized using precipitation polymerization. IIPs were synthesized using zinc sulphate and lead acetate as template, EGDMA as crosslinking agent, and methanol as porogen, MAA as functional monomer and AIBN as initiator. Polymers were characterized by FTIR for functional groups and to distinguish NIPs, IIPs washed/unwashed. IIPs were used as adsorbent to extract Zinc and lead from wastewater and honey.

The parameters that affect adsorption of ion imprinted polymer were optimized at batch mode and calculated in terms of enrichment factors. The optimum enrichment factors for Zinc ion imprinted polymer: sample pH= 7, adsorbent dose was 5 mg, contact time at 15 min and shaking speed at 100 rpm. The optimum enrichment factor for lead ion imprinted polymer: sample pH= 9, mass =50 mg, concentration =35 mg/L at 15 min.

The adsorption isotherm Langmuir and Freundlich were investigated for both zinc and lead ion imprinted polymer. The adsorption for both polymers favours Langmuir isotherms.

The selectivity study was also done, Pb (II)- ion imprinted polymers and Zn (II)- ion imprinted polymers were selective in presence of competing ions

Ion imprinted polymers are re-usable, they were evaluated 7 times and the adsorption efficiency was at 90 %. The adsorption efficiency of ion imprinted polymers were above 90%.

5.3 Recommendation

This study recommend that the material be characterized using the following techniques:

- ❖ Energy dispersive spectroscopy (EDS) for analysis of composition and constituent of IIPs/NIPs polymer that has been synthesized.
- ❖ Thermogravimetric analysis (TGA) to analyse purity, decomposition and stability of the temperature between IIPs/NIPs, stability affect the surface charge.
- ❖ Scanning electron microscopy (SEM) is used to recognized porosity and pores (cracks) form. SEM will show morphology (roughness and smoothness) of the surface differences between IIPs/NIPs.
- ❖ Brunauer-Emmett-Teller (BET) measurement will provide the pore volume and average pore diameter, where the porous and rough will indicate cavities which will distinguish between IIPs and NIPs.

Appendix



Figure A 1: Atomic absorption spectrometer

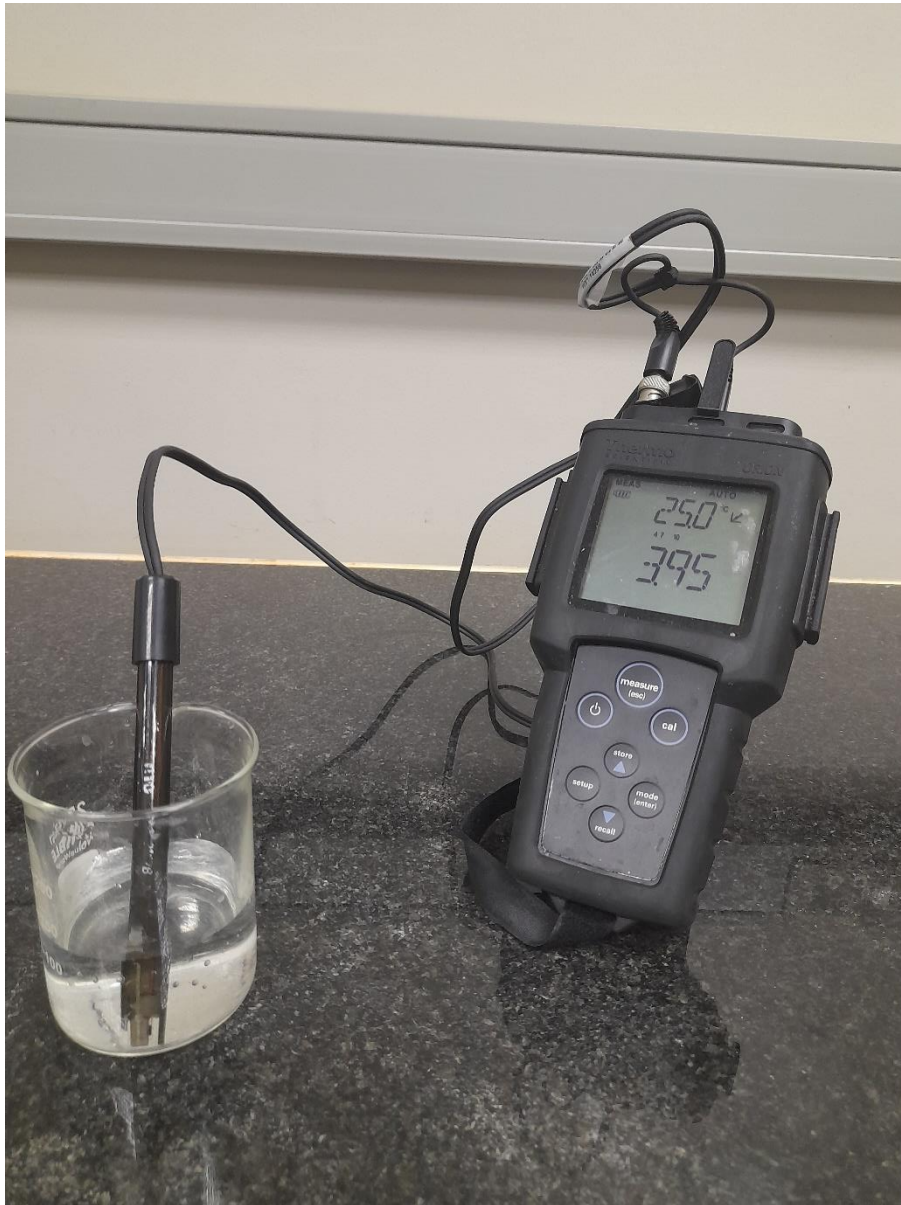


Figure A 2: pH meter

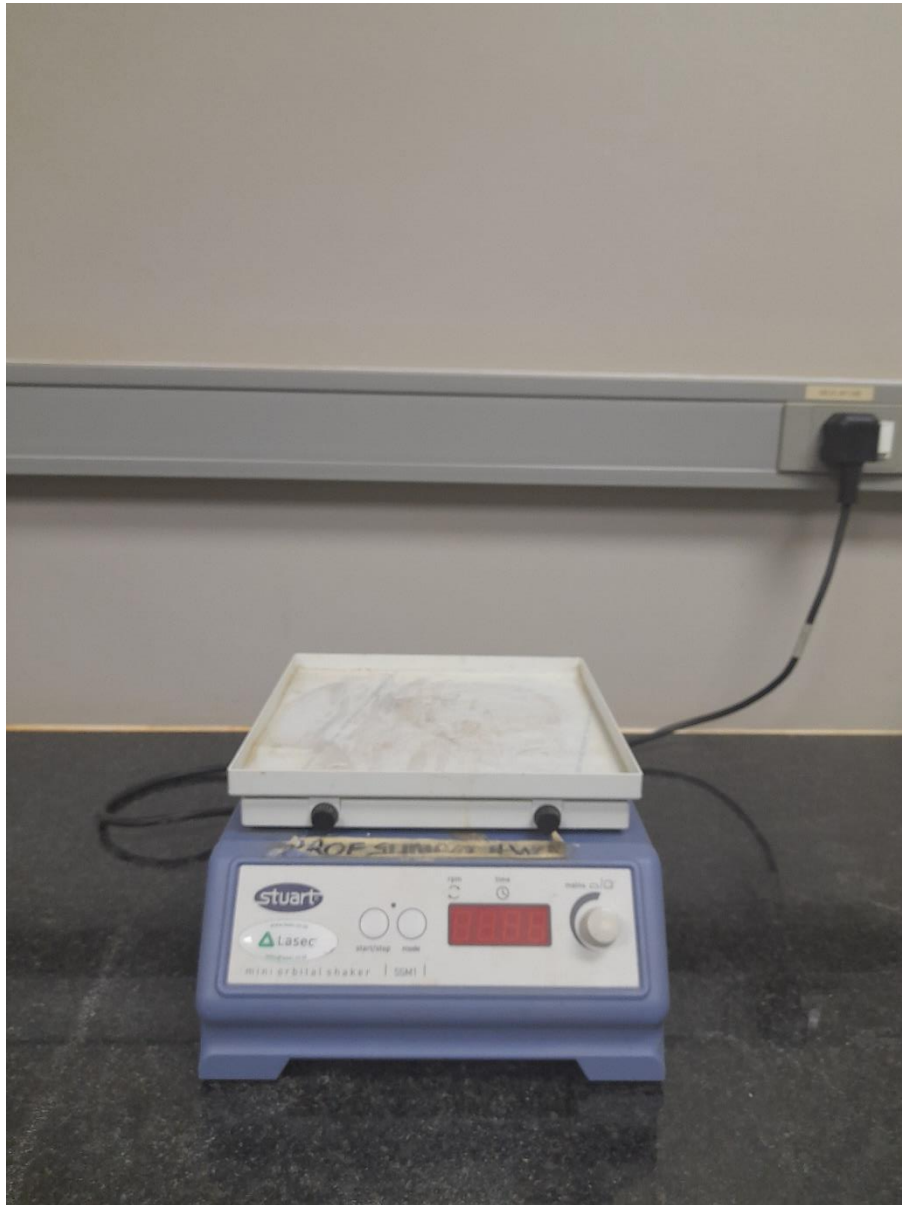


Figure A 3: Shaker



Figure A 4: Outlet



Figure A 5:Inlet



Figure A 6: Biofilter